Numerical Investigation of Microjet Impingement of Water for Cooling Photovoltaic Solar Cell

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ABSTRACT

This paper discussed the results of numerical studies of the flow field and heat transfer characteristics for a turbulent slot jet of water on photovoltaic solar cell. A wide range of various flow and geometrical parameters, with jet Reynolds number (Re) in the range of 10000-30000, and jet-to-photovoltaic distance (h) and the nozzle diameter have been considered. The results have been presented in terms of the average Nusselt numbers, and the heat transfer coefficients. The results show a significant improvement of heat transfer due to the jet impingement of water for cooling photovoltaic solar cell. An increase in the jet Reynolds number leads to an improved average Nusselt numbers increases as the nozzle-to-photovoltaic spacing decreases.

Keywords:
Photovoltaic solar cell, Numerical studies, jet impingement, Nusselt numbers, nozzle diameter

1. Introduction

Impinging cooling is an effective way to generate a high heat transfer coefficient in many engineering applications such as cooling of electronic equipment, drying of surfaces, cooling of turbine blades, laser or plasma cutting processes and steel or glass industry [1–4]. They measured free surface velocities by using the Laser-Doppler technique. The Reynolds number changing from 16,000 to 47,000 in the experimental test. Liu et al., [6] studied experimentally and numerically the cooling of uniformly heated surfaces with single phase jets and laminar circular liquid. Kazuya et al., [7] studied experimentally the influence of varying the impingement angles between the vertical planar jet and the inclined solid surface on the heat transfer characteristics of a planar free water jet impinging onto a flat substrate. The planar jet of a rectangular slot nozzle with cross section of 1.62 mm 40 mm was tested. The range of Reynolds number ranging from 2200 to 8800 based on the nozzle gap and the mean velocity. Teamah and his coworkers [8–11] investigated the heat transfer due to the impingement of circular jet on a horizontal heated surface. They tested single and multi-jets experimentally and numerically. The flow rates of water ranging from 1.5 to 8 l/min per jet. They
observed that, the jets lead to reduce the mean velocity of the fluid film for multi jets, which led to reduce of both the average local and local Nusselt number compared to the single jet. It was also noted that the overall average Nusselt number for multi jet is higher than single jet of one jet of the multi jets. Stevens and Webb [12] studied experimentally the influence of jet inclination on the local heat transfer under an obliquely impinging, round; free liquid jet striking a constant heat flux surface. The jet Reynolds number ranging from 6600 to 52,000, and jet inclination, ranging from 40 to 90. They observed that the point of maximum heat transfer shifted upstream. Whelan and Robinson [13] tested experimentally the average heat transfer coefficients and pressure drop of both impinging confined-submerged and free surface water jet arrays. Dou et al., [14] investigated the heat-transfer characteristics of the water jet on stainless steel flat plates with using inverse heat conduction methods. Karwa and Stephan [15] studied experimentally the thermo-hydrodynamic phenomenon of a hot stainless steel flat plates. The stainless steel flat plates were heated at an initial temperature of 900ºC, with a free-surface sub-cooled water jet. Lytle and Webb [16] investigated experimentally the local heat transfer characteristic by using an infrared thermal imaging technique. They found that the local Nusselt number increases as the nozzle-to-plate spacing decreases when the Reynolds number fix. A power-law relationship between the stagnation Nusselt number and the jet-to-target distance was presented. Choo et al., [17,18] studied the heat transfer characteristics of impinging jet with fixing pumping power condition at low nozzle-to-plate distance. They observed that the average Nusselt number is independent of the nozzle-to-plate spacing with fixed pumping power condition. Lee et al., [19] investigated experimentally the influence of nozzle diameter on fluid flow and heat transfer for a round turbulent jet at nozzle-to-plate distance from H/d = 2 to14. The maximum Nusselt number can be achieved when H/d = 7 where the turbulence intensity reaches roughly a maximum value. Gardon and Akfirat [20,21] found that the variation of the stagnant Nusselt number is negligible to the hump. It decreases beyond the hump. The hump moves from H/d = 6 to 2 as the Reynolds number increases.

2. Mathematical Model and Numerical Solution

2.1 Governing Equations

Figure 1 shows a schematic diagram of the geometry and the computational domain used in the present work. According to the geometrical dimensions chosen in the experimental study. The different nozzle diameters (d) 0.6, 0.8, 1.0 and 1.5 mm have been considered. In addition, the photovoltaic surface which is subjected to a constant heat flux, has negligible thickness, and is stationary. In this problem, a steady and turbulent two-dimensional flow is considered. It is also assumed that the working fluid (water) is Newtonian and incompressible. In view of the above assumptions, the governing equations of the problem are the continuity, momentum, and energy equations and the transport equations for the turbulent kinetic energy and its dissipation rate.

\[
\frac{\partial u_i}{\partial x_i} = 0
\]  

(1)

\[
\rho U_i \frac{\partial u_i}{\partial x_i} = -\frac{\partial p}{\partial x_i} + \frac{\partial}{\partial x_i}\left[ \mu \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) - \rho u_i^* u_j^* \right]
\]  

(2a)

\[
-\rho u_i^* u_j^* = \mu_t \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) - \frac{2}{3} \delta_{ij} \rho k
\]  

(2b)
\[ \rho C_p U_i \frac{\partial T}{\partial x_i} = \frac{\partial}{\partial x_i} \left[ k \frac{\partial T}{\partial x_i} - \rho \overline{u_i u_j} T_j^0 \right] \]  \hfill (3)

The turbulent viscosity term \( \mu_t \) is to be computed from an appropriate turbulence model. The expression for the turbulent viscosity is given as

\[ \mu_t = \rho C_{\mu} \frac{k^2}{\varepsilon} \]  \hfill (4)

In the present study, k–\( \varepsilon \) RNG turbulence model is used as follows

\[ \frac{\partial}{\partial x_i} \left( \rho k \overline{u_i} \right) = \frac{\partial}{\partial x_j} \left[ \left( \mu + \frac{\mu_t}{\sigma_k} \right) \frac{\partial k}{\partial x_j} \right] + G_k - \rho \varepsilon \]  \hfill (5)

Similarly, the dissipation rate of TKE, \( \varepsilon \) is given by the following equation.

\[ \frac{\partial}{\partial x_i} \left( \rho \varepsilon \overline{u_i} \right) = \frac{\partial}{\partial x_j} \left[ \left( \mu + \frac{\mu_t}{\sigma_k} \right) \frac{\partial \varepsilon}{\partial x_j} \right] + C_{1\varepsilon} \frac{\varepsilon}{k} G_k - C_{2\varepsilon} \rho \frac{\varepsilon^2}{k} \]  \hfill (6)

Where \( G_k \) is the rate of generation of the TKE while \( \rho \varepsilon \) is the destruction rate. \( G_k \) is written as

\[ G_k = \left( -\rho \overline{u_i u_j} \right) \frac{\partial \overline{u_j}}{\partial x_i} \]  \hfill (7)

2.2 Boundary Conditions

The boundary conditions applied in the present work are illustrated in Figure 1. As shown in this figure, a velocity-inlet boundary condition at constant temperature (298 K) is assumed at the jet exit with a velocity magnitude compatible with the jet exit Reynolds number. The inlet turbulence intensity and hydraulic diameter were set to be 5% and 2d respectively. The thermal boundary condition at the photovoltaic surface is a constant heat flux. Also, at the flow outlet, the pressure-outlet boundary condition has been assumed.

Fig. 1. Schematic of slot-jet impingement cooling scheme on photovoltaic solar panel
To attain accurate prediction in the circular tube, the standard $k-\varepsilon$ turbulence model, the Renormalized Group (RNG) $k-\varepsilon$ turbulence model were selected. The time-independent incompressible Navier-Stokes equations and the turbulence model analysis were solved using finite volume method. To evaluate the pressure field, the pressure-velocity coupling algorithm SIMPLE (Semi Implicit Method for Pressure-Linked Equations) was selected. The solutions are considered to be converged when the normalized residual values reach $10^{-5}$ for all variables.

3. Results and Observations

3.1 Effect of Nozzle Photovoltaic Cell Spacing

The numerical study was conducted to study the effect of jet impingement of water for cooling photovoltaic solar cells. The different nozzle-to-photovoltaic spacing of 10, 20, 30 and 40mm was studied with different Reynolds number at different nozzles size. Figure 2 shows the variation of Nusselt number with Reynolds number. From the results, it is clearly noted that the Nusselt number increases with the rise of Reynolds number for all spacing. The Nusselt number also increases with the decrease of the nozzle-to-photovoltaic spacing and has a maximum value at the spacing of 10mm for $d=0.6$ case. This can be explained by a high heat transfer coefficient and rapid mixing flow can be achieved when the photovoltaic solar cell closes to the nozzle.

![Graph showing variation of Nusselt number with Reynolds number](image)

**Fig. 2.** Variation of the Nusselt number with Reynolds number for different nozzle-to-photovoltaic cell spacing at $d=0.6\text{mm}$

Figure 3 shows the variation of Nusselt with Reynolds numbers at different nozzle-to-photovoltaic cell spacing of 10, 20, 30 and 40mm at $d=0.8\text{mm}$. It is observed that the Nusselt number increases with the rise of Reynolds number for all spacing. The Nusselt number also increases with the decrease of the nozzle-to-photovoltaic cell spacing. It can be seen that the high values of average Nusselt number occur in the jet impingement the nozzle-to-photovoltaic cell spacing is 10mm.
Figure 4 shows the variation of Nusselt number with Reynolds number at different nozzle-to-photovoltaic spacing of 10, 20, 30 and 40mm at d=1mm. As can be seen from this figure, increasing the jet Reynolds number, will increase the inlet velocity. This will lead to the average Nusselt number increase significantly. The Nusselt number also increases with the decrease of the nozzle-to-photovoltaic spacing. It can be seen that the high values of average Nusselt number occur in the jet impingement the nozzle-to-photovoltaic spacing at 10mm.
Figure 5 shows the variation of Nusselt number with Reynolds number at different nozzle-to-photovoltaic spacing of 10, 20, 30 and 40mm at d=1.5mm. From the results, it is clearly noted that the Nusselt number increases with the rise of Reynolds number for all spacing. The Nusselt number also increases with the decrease of the nozzle-to-photovoltaic spacing and has a maximum value at the spacing of 10mm for d=1.5 case. This can be explained by a high heat transfer coefficient and rapid mixing flow can be achieved when the photovoltaic solar cell is close to the nozzle.

![Graph of Nusselt number vs Reynolds number](image)

**Fig. 5.** Variation of the Nusselt number with Reynolds number for different nozzle-to-photovoltaic cell spacing at d=1.5mm

### 3.2 Effect of Nozzle Diameter

Figure 6 shows the variation of the Nusselt number with Reynolds number for different nozzle diameter at H=10mm. According to the results, it is clearly seen that the Nusselt number increases with the rise of Reynolds number for all nozzle diameter. The Nusselt number also increases with the increase of the nozzle diameter and has a maximum value at the d=1.5.

### 3.3 Effect of Different Reynolds Number on The Local Heat Transfer Coefficient

Figure 7 shows the variation of local heat transfer coefficient with X(m) at different Reynolds number with nozzle-to-photovoltaic spacing of 10mm at d=0.8mm. From the results, it is clearly noted that the heat transfer coefficient increases with the rise of Reynolds number. Figure 8 shows the variation of heat transfer coefficient with X(m) at different Reynolds number with nozzle-to-photovoltaic spacing of 10mm at d=1.5mm. From the results, it is clearly shown that the heat transfer coefficient increases with the rise of Reynolds number.
**Fig. 6.** Variation of the Nusselt number with Reynolds number for different nozzle diameter at H=10mm

**Fig. 7.** Variation of the local heat transfer coefficient with X at d=0.8 mm and H=10mm
4. Conclusions

The effects of using jet impingement of water on the heat transfer field due to cooling a photovoltaic solar cell were numerically analysed. The impacts of the nozzle diameter, Reynolds numbers, and jet-to-photovoltaic distances on the heat transfer of jet water have been discussed in detail. The outcomes indicate that by increasing the jet Reynolds number and decreasing the jet-to-target space, the target surface temperature is reduced which results in enhancement of the average Nusselt number distribution. Hence, the average Nusselt numbers increase as the nozzle increases. It is also found that the average Nusselt numbers increases as the nozzle-to-photovoltaic spacing decreases because jet Reynolds number increasing led to increase the heat transfer coefficients. Also, it is clearly noted that the heat transfer coefficient increases with the rise of Reynolds number. The Nusselt number considerably increased with increasing Reynolds number, \( Re \) in the range of 10000-30000.

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