

Flow Characteristics of Disk Bypass Pipeline Inspection Gauge (PIG) in Natural Gas Pipelines using Computational Fluid Dynamics

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ABSTRACT

Disk bypass pipeline inspection gauge (PIG) is considered as an efficient device for pigging operations including cleaning, maintaining and inspecting pipelines. The PIG performance is influenced by the fluid flow characteristics as PIG moves forward due to differential pressure of fluid around the PIG. This study focuses on flow characterization of fluid around disk bypass PIG for natural gases pipelines including methane, ethane, and butane using computational fluid dynamics approach. The control volume method with steady state Turbulent k- ϵ model was applied for simulation purposes using ANSYS Fluent 19 software. Fluid velocities at different sections around PIG and differential pressure were investigated for various bypass opening percentages. The results showed that by increasing bypass opening percentages from 5% to 15%, fluid velocity at bypass opening section has reduced 28.28%, 40.43%, and 21.21% for ethane, butane, and methane, respectively, while differential pressure reduced 88%, 86% and 89%. This indicated that 15% bypass opening percentage provided the best flow characteristics among all cases considered. At 15% bypass opening percentage, methane resulted in the lowest fluid velocity at bypass opening section and lowest differential pressure compared to others. Additionally, a correlation of differential pressure of these gases as a function of bypass opening percentage and other parameters was also developed for first time. All results are important for design selection of PIG parameters for efficient pigging operation.

1. Introduction

Pipeline inspection gauge (PIG) is a device used in oil and gas industries to perform pigging operations including liquid removal, cleaning debris, and inspecting pipelines [1-5]. These operations cannot be done properly if the PIG moves too quickly in addition to the risk of damaging the pipeline walls and the PIG itself [6-8]. The PIG speed is therefore considered as one of the most important concerns in pigging operations and remains a big challenge in oil and gas industries.

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The PIG movement is greatly influenced by the pipeline flow characteristics as the PIG propels inside the pipeline due to differential pressure developed between its tail and front [9-11]. Therefore, the flow characteristics of fluid inside the pipeline including the fluid velocity and pressure need to be determined properly in order to control the PIG speed in pigging operations [6,12]. Additionally, new designs of PIG have evolved from time to time in order to achieve better control of PIG speed and movement towards improving the pigging performance. Among the important developments was the introduction of a bypass hole in the PIG body through which fluid can pass [9,13,14]. This type of PIG, namely the bypass PIG, allows the control the PIG speed without affecting the pipeline production rate. In more recent development, a disk was introduced in front of the bypass opening section which reduces the fluid pressure at this section, and therefore controls PIG speed to be in moderate range [6].

A number of experimental and numerical studies on bypass PIG have been reported in literature with only few has considered disk bypass PIG as the latter was introduced more recently. A pigging operation has been simulated using a model that combines the equation of the PIG to the energy, momentum, and mass equations for the fluid flow [12,15-17]. Utilizing the commercial computational fluid dynamics (CFD) software, ANSYS Fluent, Singh and Henkes [18] analysed a simple bypass PIG model for both single-phase and two-phase flow.

Zhang *et al.*, [12] carried out a numerical study on bypass PIG in the medium of water and crude oil. The study found that as the bypass hole diameter raised from 0.1 to 0.5 m under the specific research conditions, the PIG speed was reduced from 2.777 to 0.373 m/s for crude oil and from 2.779 to 0.589 m/s for water. This study concluded that the PIG speed was lowest in crude oil. Meanwhile, and Liu *et al.*, [8], Hendrix *et al.*, [7], Hendrix *et al.*, [19], Hendrix *et al.*, [20], also conducted CFD analyses on bypass PIG to predict the PIG speed. All these numerical studies considered only one type of natural gas for single-phase flow to conduct the analyses. None of the studies has considered several different gases in their analyses from which comparison of flow characteristics and PIG performance can be done.

In terms of experimental works, several studies have been performed using bypass PIG. Wang *et al.*, [1] conducted an experimental study on bypass PIG and regular PIG for wax removal in oil flowing pipelines. Comparisons were done between the two types of PIGs and the results revealed the significantly different performances between the two PIGs. Meanwhile, Zhu *et al.*, [14] conducted an experimental study on dynamics of rotatable bypass valve for gas pipelines to control the PIG speed. In this experiment, the relationship between differential pressure over the bypass valve, bypass valve opening, and torque can be acquired, which can provide references to PIG control algorithms.

Additionally, experiment works on bypass PIG prototype for gas pipelines has been performed by Chen *et al.*, [10] wherein an infrared ray-based PIG velocity detection method was proposed. The results revealed that the average velocity of bypass PIG shifted linearly with the flow rate of the rear driving gas and no variation can be noticed in gas-to-PIG velocity whenever the bypass fraction was the same. With the presence of bypass fraction, the PIG speed reduced significantly and at the same time alleviated the movement fluctuation of the PIG. Moreover, Hendrix [11], Zhu *et al.*, [21] and Chen *et al.*, [22] also conducted experimental studies on bypass PIG to measure PIG speed and friction forces.

For studies involving disk bypass PIG, only very few were identified in the literature. Among these studies, one study was performed by Korban [23] who considered disk bypass PIG along with conventional and complex bypass PIGs for single-phase condition of gas flow by using ANSYS Fluent (version 14.5). In his study, two dimensional axisymmetric CFD model was utilized to evaluate the flow of the considered PIGs for oil and gas industry. In addition, the relationship between the governing parameters and the overall coefficient of pressure loss of the bypass PIG were evaluated

by conducting various parametric studies. Liang [6] and Korban [23] also conducted a CFD analysis for conventional PIG, disk bypass PIG, and complex PIG for single and multiphase gas flow. Correlations of pressure loss coefficient with governing parameters were developed for these different types of PIG which showed good agreement with Idelchik and Fried's [24] correlation for a thick orifice. Hendrix [11] and Hendrix *et al.*, [20] also studied disk bypass PIG to analyse pressure loss coefficient and friction forces for gas pipelines. According to the studies by Korban [23], Liang [6] and Azpiroz *et al.*, [25] bypass PIG with disk provided better performance to control and reduce PIG speed compared to bypass PIG without disk. Due to the presence of the disk in front of the bypass opening section, the bypass opening area can be controlled to be smaller than the bypass entry section thereby controlling and reducing the PIG speed [6].

The review of these studies revealed that only very few studies have been done on disk bypass PIG for natural gas transporting pipelines. To the best of the authors knowledge, none of the studies has performed analyses to compare the flow characteristics of disk bypass PIG in different natural gases such as ethane, butane and methane. These natural gases are however among the common fluids transported in oil and gas industries. Therefore, it is important to investigate the flow characteristics of these gases towards improving the pigging performance using PIG. In this regard, analysis using disk bypass PIG is desired since recent studies have shown its improved performances in comparison to bypass PIG without disk. Therefore, the aim of the current study was to analyse the flow characteristics of disk bypass PIG in terms of fluid velocities and differential pressure for natural gases pipelines including methane, ethane, and butane. The velocity contours and streamline as well as pressure contour in the presence of disk bypass PIG are presented for better understanding of the flow characteristics. Additionally, a correlation of differential pressure in terms of bypass opening percentages of the PIG and other parameters for these gases was also developed for first time towards providing more valuable insights into improving pigging operations in oil and gas industries.

2. Methodology

Computational fluid dynamics (CFD) analysis using ANSYS Fluent 19 software was performed in this study to analyse the flow characteristics of disk bypass PIG in the considered natural gas pipelines. In this section, firstly the equations governing the motion of the flow is presented including the model for turbulent flow as well as the PIG fluid dynamics. This is followed by the description of the computational model including the boundary conditions and the parameters considered in this study.

2.1 Governing Equations

2.1.1 Navier-stokes equations

For the motion of viscous fluids, the Navier-Stokes equation is considered as governing equation which was derived from Newton's second law of motion. In this study, the fluids were considered incompressible since the pressure variation of the fluids in pipeline is small compared to the absolute pressure. The gases considered in this study were assumed to be incompressible Newtonian fluids as during flowing through the pipe the viscosities of the gases were considered constant with zero shear rate at zero shear stress. For incompressible Newtonian fluids the widely used Navier-Stokes equation is given as

$$\rho \left(\frac{\partial \vec{u}}{\partial t} + \vec{u} \cdot \nabla \vec{u} \right) = -\nabla P + \mu \nabla^2 \vec{u} + \vec{f} \quad (1)$$

where ρ is the fluid density; \vec{u} is the velocity vector of three-dimensional fluids which represents the velocities in x, y and z direction (u, v and w); P is the fluid pressure; μ is the viscosity of the fluid and \vec{f} is the body forces acting on the fluid such as gravitational force. Additionally, for the incompressible fluids the general continuity equation, which was derived from mass conservation in the system, can be presented as

$$\nabla \cdot \vec{u} = 0 \quad (2)$$

2.1.2 The $k - \epsilon$ turbulence model

The $k - \epsilon$ turbulence model is considered as the most common and applied turbulence model which has also been applied in the current study. Most of recent numerical studies that dealt with turbulent flow applied $k - \epsilon$ turbulence model including the work by Liang [6] and Talbizadeh and Keshtkar [31] for disk bypass PIG simulation [26-30]. Therefore, $k - \epsilon$ turbulence model was considered for this study also. This model consists of two equations which are turbulent kinetic energy and dissipation rate derived from the Boussinesq eddy viscosity and transport equation. The equation for Boussinesq eddy viscosity can be derived from the following equation which is related to Reynolds stress tensor as well [32].

$$-\rho \overline{u'_i u'_j} = \mu_t \left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) - \frac{2}{3} \rho k \delta_{ij} \quad (3)$$

where $k = \frac{1}{2} u'_i u'_i$ is the turbulent kinetic energy, u' is the root mean square of the fluctuating velocities, U is the mean velocity, μ_t is the turbulent eddy viscosity, and the term δ_{ij} is the Kronecker delta. Meanwhile, the turbulent eddy viscosity is defined by the following equation

$$\mu_t = \rho C_\mu \frac{k^2}{\epsilon} \quad (4)$$

where ϵ is the turbulence dissipation rate and C_μ is a constant.

The transport equation for turbulence kinetic energy is presented in following equation [24]

$$\frac{\partial}{\partial t} (\rho k) + \frac{\partial}{\partial x_i} (\rho k u_i) = \frac{\partial}{\partial x_j} \left[\left(\mu + \frac{\mu_t}{\sigma_k} \right) \frac{\partial k}{\partial x_j} \right] + G_k + G_b - \rho \epsilon - Y_M + S_k \quad (5)$$

where G_k is the turbulence kinetic energy production amount for the actual gradients of velocity; G_b is the turbulence kinetic energy generation amount due to buoyancy force whereby in the current study $G_b = 0$ since heat transfer is not taken into consideration; the fluctuating dilation is referred as Y_M which is utilized for compressible fluid only and is ignored for incompressible fluid; σ_k is the turbulent Prandtl number for k while S_k is a user-defined source term. The term G_k can be expressed by the following equation

$$G_k = -\rho \overline{u'_i u'_j} \frac{\partial u_j}{\partial x_i} \quad (6)$$

The transport equation for turbulence dissipation rate is given by Versteeg and Malalasekera [32].

$$\frac{\partial}{\partial t}(\rho\epsilon) + \frac{\partial}{\partial x_i}(\rho\epsilon u_i) = \frac{\partial}{\partial x_j} \left[\left(\mu + \frac{\mu_t}{\sigma_\epsilon} \right) \frac{\partial \epsilon}{\partial x_j} \right] - \rho C_{2\epsilon} \frac{\epsilon^2}{k} + C_{1\epsilon} \frac{\epsilon}{k} (G_k + C_{3\epsilon} G_b) + S_\epsilon \quad (7)$$

where $C_{1\epsilon}$, $C_{2\epsilon}$ and $C_{3\epsilon}$ are constants, σ_ϵ is the turbulent Prandtl number for ϵ and S_ϵ is a user-defined source term. For the model of realizable $k - \epsilon$, the values for these constants were taken as follows [4]:

$$C_{1\epsilon} = 1.44; C_{2\epsilon} = 1.92; C_\mu = 0.09; \sigma_k = 1.0; \text{ and } \sigma_\epsilon = 1.3$$

2.1.3 Fluid dynamics of PIG

PIG motion in a pipeline is usually determined by force balance between the frictional force and driving pressure force F_p . By using a control volume analysis through the entire PIG, F_p can be denoted as $F_p = \Delta P A$ where ΔP is the differential pressure over the PIG, i.e., between its downstream and upstream, while A is the cross-sectional area of the pipe. The differential pressure ΔP is expressed as

$$\Delta P = P_{up} - P_{down} \quad (8)$$

where P_{up} and P_{down} represent the pressure at each side (upstream and downstream) of the PIG. An equation of force balance is usually applied to obtain motion of PIG with fluid flow over the pipeline which is given by Talbizadeh and Keshtkar [31].

$$m \frac{dv}{dt} = (P_{up} - P_{down}) A - mg \sin \theta - F_c \quad (9)$$

where v and m are the velocity and mass of the PIG, respectively; F_c is the axial contact force acting on PIG; θ is the inclination angle of PIG movement direction with respect to horizontal axis which is zero for this study; and g is the gravitational acceleration.

2.2 Computational Model and Boundary Conditions

A two-dimensional axisymmetric pipe with disk bypass PIG was modelled in this study using ANSYS Fluent 19 software as shown in Figure 1. For simulation purpose, the model was considered as a stop condition during movement through the pipeline. The control volume method for single-phase steady state turbulent flow was employed. The flow region of fluid inside the whole pipeline was assumed turbulent and the Reynolds number was 58786 for ethane, 151958 for butane and 26569 for methane, respectively. At inlet, velocity inlet with room temperature was considered. Meanwhile, the boundary condition at outlet was set to be pressure outlet and gauge pressure was considered. In this model, the PIG was considered to be completely coupled with the pipe wall. Meanwhile, the pipe wall was considered stationary with no-slip condition. Moreover, pressure velocity coupling scheme was considered simple (steady state) solution method while spatial discretization of pressure, momentum, turbulent kinetic energy and turbulent dissipation rate were considered second order unpinning solution method under relaxation factor 0.7 for momentum, 0.8 for turbulent kinetic energy, 0.8 for turbulent dissipation rate and 1 for turbulent viscosity.

To analyse the flow characteristics of the natural gases in terms of its velocity, the fluid velocities at different positions were considered as illustrated in Figure 1, i.e., v_1 was taken as the fluid velocity at the bypass entry section, v_2 represented the fluid velocity at the horizontal bypass section, while

v_3 indicated the fluid velocity at the bypass opening section. Meanwhile, to determine the differential pressure of the flow, pressures at two locations were considered as mentioned previously, i.e., P_{up} at the upstream and P_{down} at the downstream. The parameters shown in Figure 1 are described in the next section.

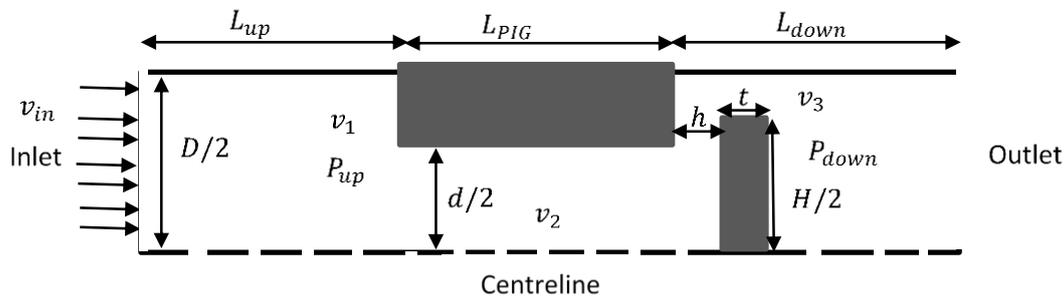


Fig. 1. Geometry of disk bypass PIG

2.3 Parameters of PIG and Properties of Natural Gases

The parameters of the disk bypass PIG as well as the pipe as shown in Figure 1 are provided in Table 1 while the fluid dynamics properties of the natural gases considered in this study are shown in Table 2. As seen in Figure 1, the disk bypass PIG has a disk with diameter of H in front of the bypass section that makes the fluid opening area smaller than the entry and bypass section of the PIG. The distance between the disk and main body of the bypass PIG is referred to as the bypass opening section. For convenience, it is represented in terms of percentage, namely bypass opening percentages, h (unit of %). In this study, five different bypass opening percentages were considered as shown in Table 1 in order to investigate the resulting flow characteristics of the PIG.

Table 1

Parameters of pipe disk bypass PIG as shown in Figure 1

Parameters (unit)	Value
Pipe diameter, D (mm)	460
Horizontal bypass PIG diameter, d (mm)	195
Upstream pipe length, L_{up} (mm)	$5 D$
Downstream pipe length, L_{down} (mm)	$20 D$
Horizontal bypass length, L_{PIG} (mm)	610
Disk diameter, H (mm)	270
Disk thickness, t (mm)	25
Bypass opening percentages, h (%)	5, 7.5, 10, 12.5 and 15
Inlet velocity of gases, v_{in} (m/s)	0.94

Table 2

Fluid dynamic properties of ethane, butane and methane

Property	Ethane	Butane	Methane
Density, ρ (kg/m ³)	1.263	2.46	0.6679
Viscosity, μ (kg/m.s)	9.29×10^{-6}	7×10^{-6}	1.087×10^{-5}
Reynolds number (Re)	58786	151958	26569

2.4 Grid Independency Test

One of the important aspects of computational model and simulation is the grid independency test to determine the optimum number of nodes needed for the simulation. For this purpose, a

representative case of 10% bypass opening percentage was considered and five different grid sizes as shown in Table 3 were used in this test to analyse the effect of the turbulent kinetic energy at the bypass opening section for methane. Two-dimensional structured orthogonal mesh was used in Ansys Fluent meshing tool wherein the minimum orthogonal mesh quality was 0.999512. Since the minimum orthogonal mesh quality obtained was close to 1, it can be concluded that the mesh quality used in this study was good. However, the results are shown in Figure 2, which demonstrates that there is no significant difference between Grid-4 and Grid-5. Therefore, for this study, Grid-4 has been used for all simulations.

Table 3

Grid number and number of nodes used as meshing for grid independency test with methane as case study

Grid no.	Number of nodes	Turbulent Kinetic Energy (J/kg)
Grid-1	300206	0.014
Grid-2	332066	0.011
Grid-3	378096	0.0096
Grid-4	404451	0.009
Grid-5	414456	0.009

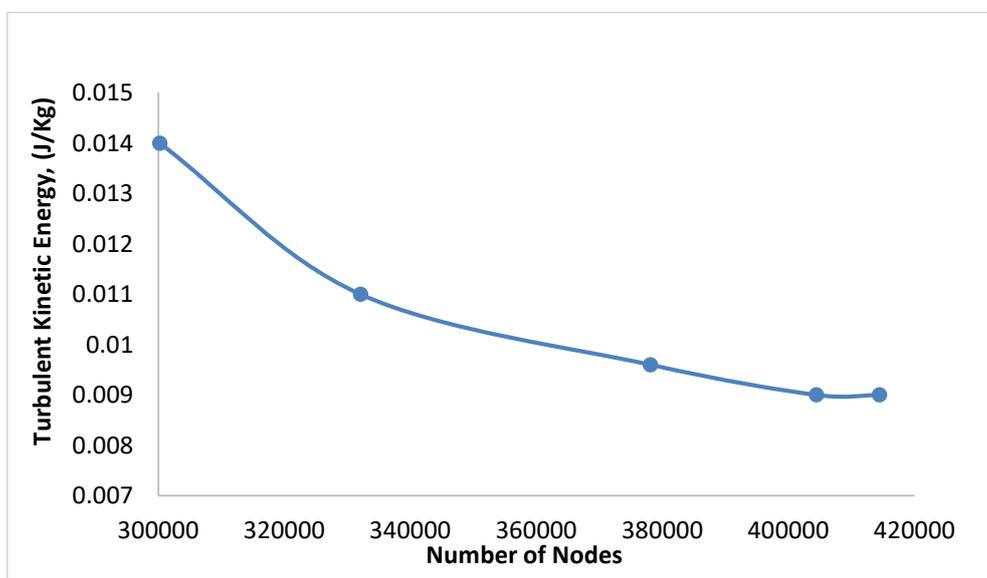


Fig. 2. Turbulent kinetic energy of disk bypass PIG with 10% bypass opening percentage as function of various grids used in grid independency test for methane as study case

2.5 Validation

To justify any numerical model, validation is mandatory. For this purpose, the theory of pressure loss coefficient for disk bypass PIG derived by Liang [6] was considered. The pressure loss coefficient was calculated from current CDF model and validated by using the pressure loss coefficient observed from theory. Butane with 7.5%, 10%, 12.5% and 15% bypass opening percentage was considered as representative fluid. The results are presented in Figure 3 which demonstrates that pressure loss coefficient between theory and current CFD study showed good agreement within maximum deviation below 10%. The equation is given below:

$$K'_{dp} = 0.5 \left(1 - \frac{d^2}{D^2} \right)^{3/4} + 2 \frac{H}{d} + \frac{0.155d^2}{h^2} - 1.85 \quad (10)$$

where, K'_{dp} represents pressure loss coefficient for bypass PIG. Additionally, d , D , H and h represent diameter of bypass section, diameter of main pipe, height of disk and distance of disk from PIG body, respectively.

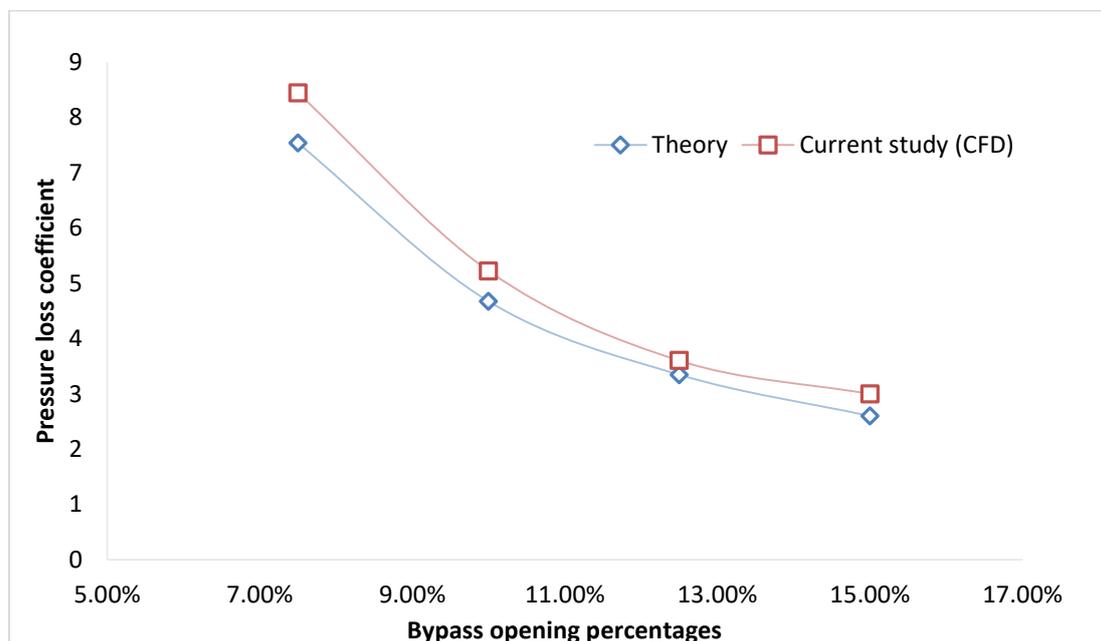


Fig. 3. Comparison of pressure loss coefficient between theory and CFD model for validation purpose

3. Results

In this study, simulations using the computational approach were undertaken to analyse the flow characteristics of the considered fluids around the disk bypass PIG. The results were generated and analysed in terms of the fluid velocities at different sections of the PIG, i.e., bypass entry section (v_1), horizontal bypass section (v_2), and bypass opening section (v_3). These velocities are important as the PIG movement is greatly influenced by the pipeline flow characteristics [9,11,22]. Additionally, differential pressure was also investigated in this study since the PIG moves due to this differential pressure which is generated by the fluid around the PIG between its upstream and downstream. It is one of the key factors to predict PIG speed inside pipelines and therefore the results of differential pressure are reported in this study as part of the flow characterization of the disk bypass PIG [4].

In this study, the effects of bypass opening percentage on these velocities and differential pressure were also analysed to provide more understanding of this important feature on how it influences the flow characteristics around the PIG. Additionally, the correlation of differential pressure in terms of PIG bypass opening percentage as well as other parameters was also developed for first time to enable its prediction which is important in oil and gas pigging operations involving natural gases.

3.1 Velocity of Different Natural Gases Around Disk Bypass PIG

Figure 4 to Figure 6 show the fluid velocities of ethane, butane, and methane at bypass entry section (v_1), horizontal bypass section (v_2) and bypass opening section (v_3) respectively, as a function of the bypass opening percentage. It can be seen from Figure 5 that for all gases v_1 did not change much as the bypass opening percentage increased. This was expected since the changes in bypass

opening percentage did not affect the flow area at bypass entry section. Additionally, among the three gases considered in this study, methane provided the highest velocity at the bypass entry section, v_1 and the lowest velocity at the horizontal bypass section, v_2 . This is due to the fluid dynamics properties of these gases. Compared to butane and ethane, methane has the lowest density and highest viscosity which make the Reynolds number of methane lowest. According to the fluid mechanics theory of Reynolds number, increase of viscosity causes reduction of fluid velocity and similarly decrease of density also causes reduction of fluid velocity.

Meanwhile, Figure 6 shows the fluid velocity at the bypass opening section, v_3 . It can be observed from this figure that v_3 reduced as the bypass opening percentage increased for all the gases considered in this study. This is expected due to the presence of disk at the bypass opening section which affects the flow area in that section. As a result, v_3 was lowest at the highest bypass opening percentage which was 15% as seen in Figure 6. The bypass opening percentage which indicates the distance between the disk and the PIG main body causes reduction of fluid velocity at this section. By increasing the bypass opening percentages from 5% to 15%, fluid velocity at v_3 has reduced 28.28%, 40.43%, and 21.21% for ethane, butane, and methane, respectively. These results indicated that bypass opening percentage of 15% provided the best flow characteristics in terms of velocity reduction in comparison to other percentages. This finding is important for better parameter selection of the PIG to achieve more efficient pigging performance.

Among the three gases, methane showed 5-21% lower velocity at v_3 compared to ethane (for h values from 15% reduced to 5%) while 11-33% lower velocity at v_3 compared to butane. Methane has the lowest density and highest viscosity compared to ethane and butane which is the main reason for the lowest fluid velocity of methane at v_2 and v_3 compared to other gases.

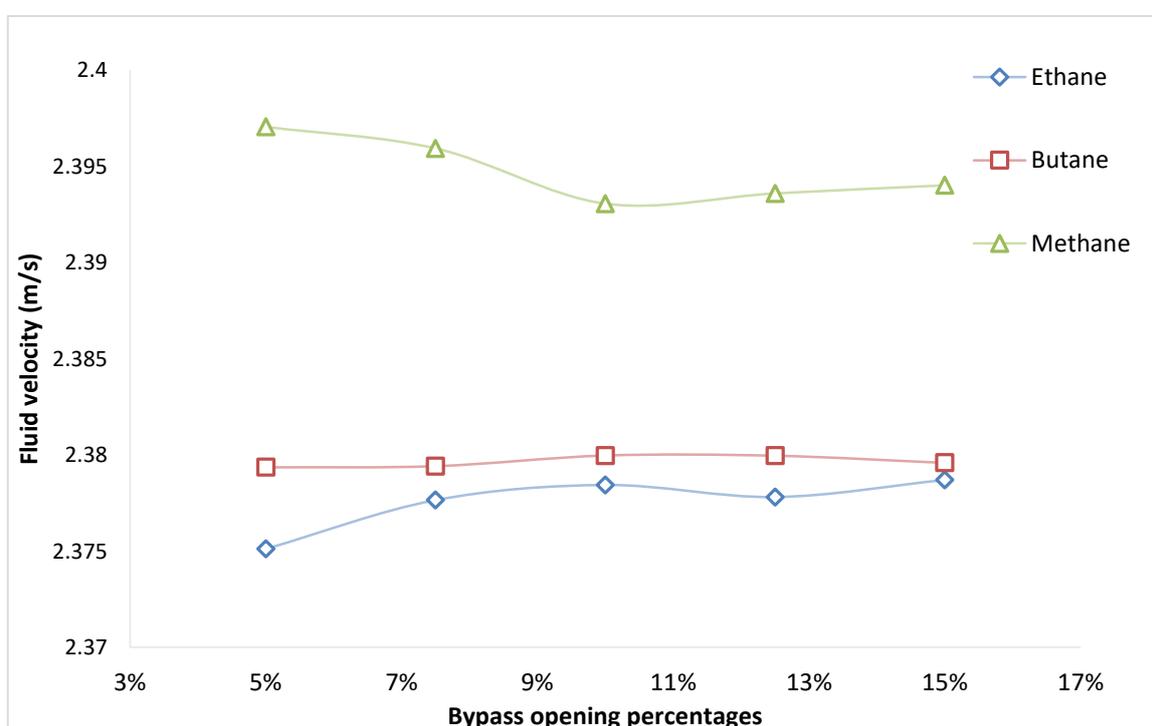


Fig. 4. Velocity at bypass entry section, v_1 as a function of bypass opening percentages for ethane, butane and methane

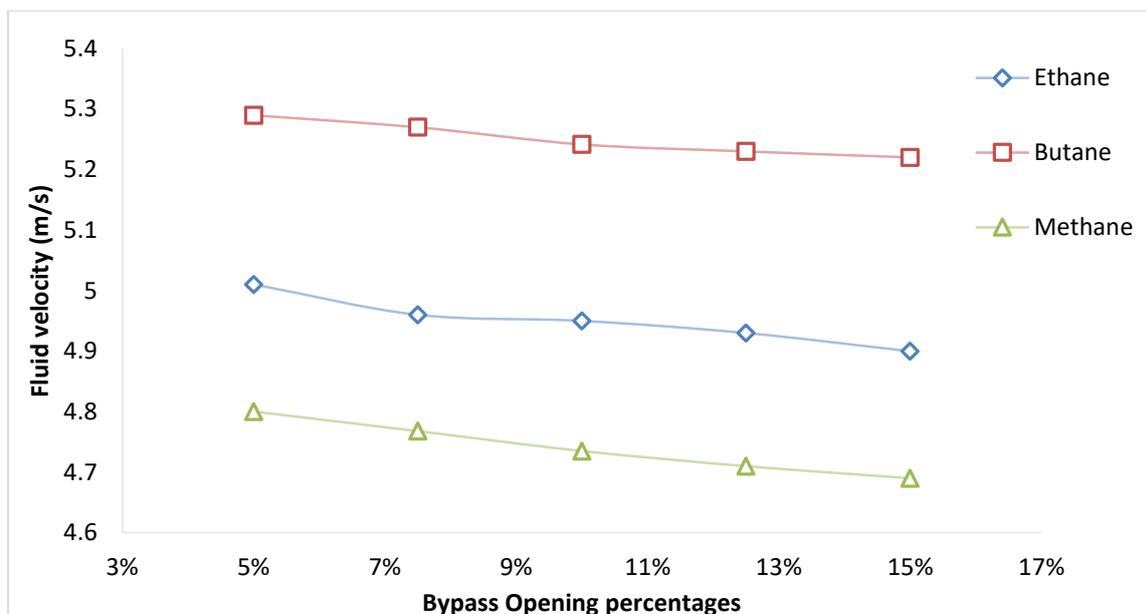


Fig. 5. Velocity at horizontal bypass section, v_2 as a function of bypass opening percentages for ethane, butane and methane

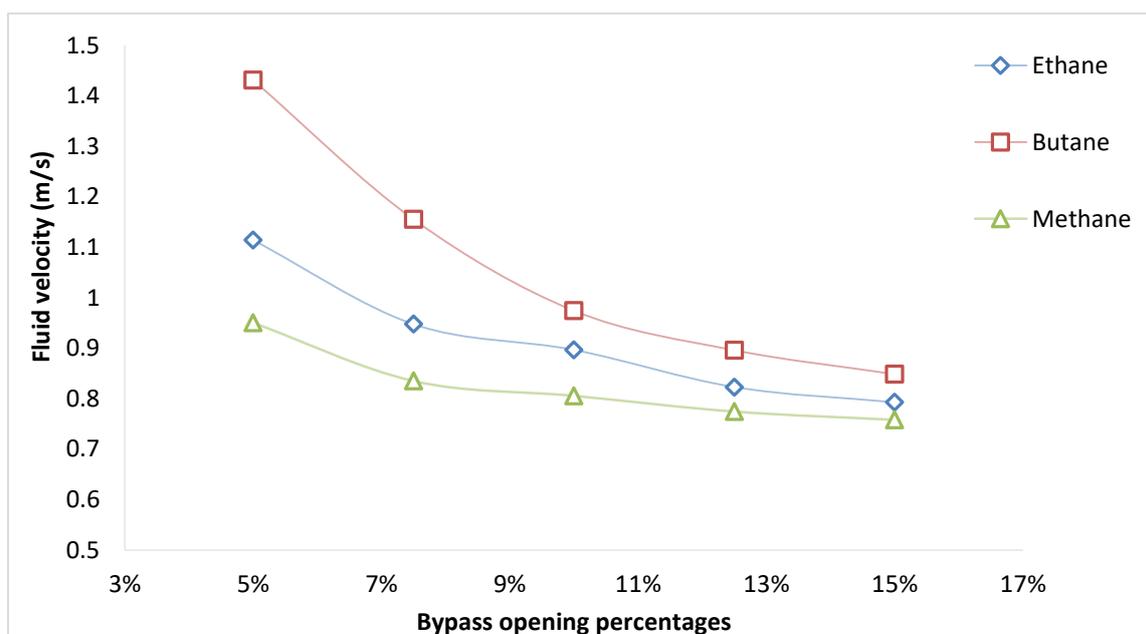


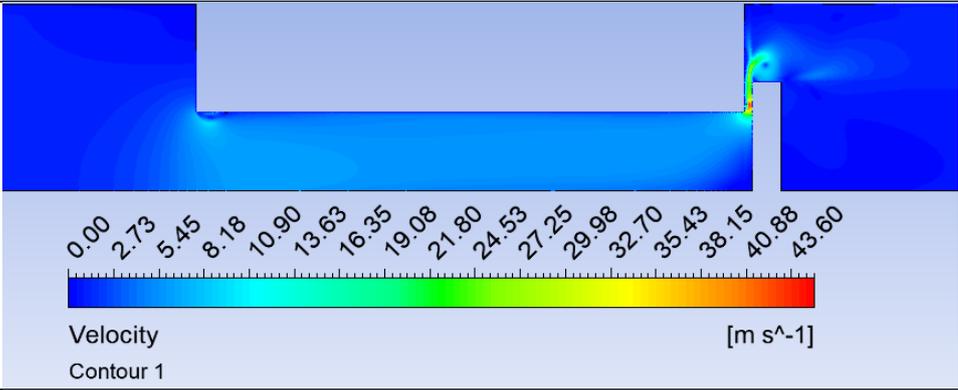
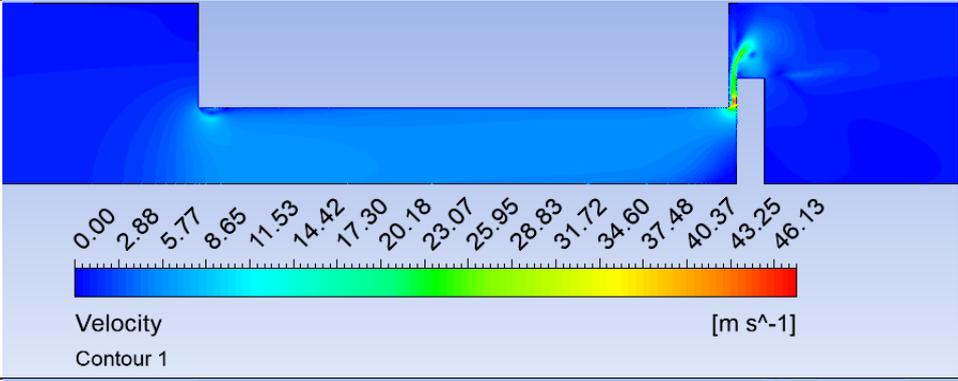
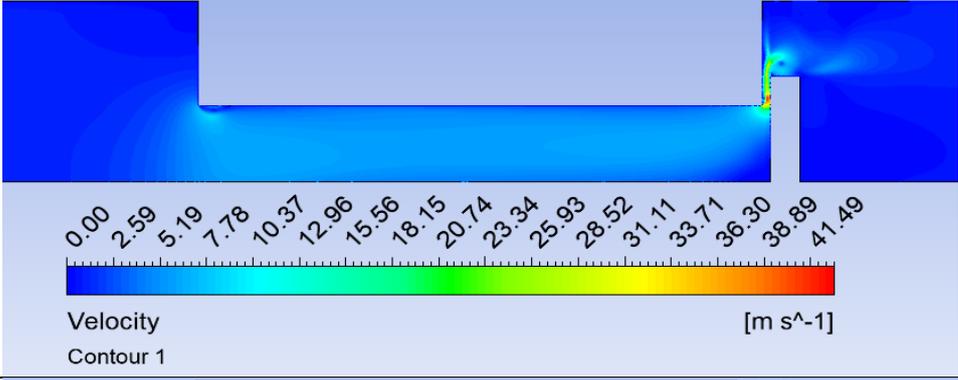
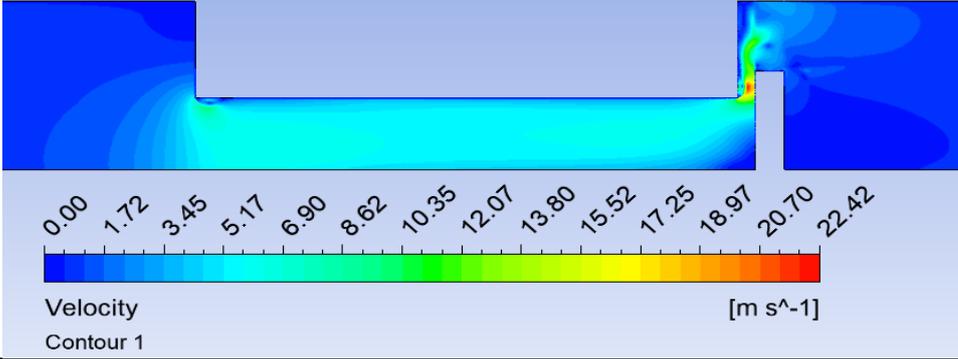
Fig. 6. Velocity at bypass opening section, v_3 as a function of bypass opening percentages for ethane, butane and methane

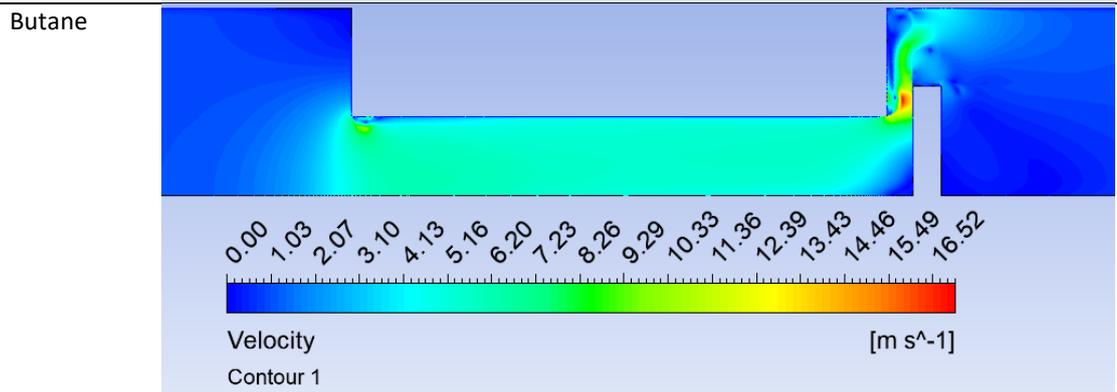
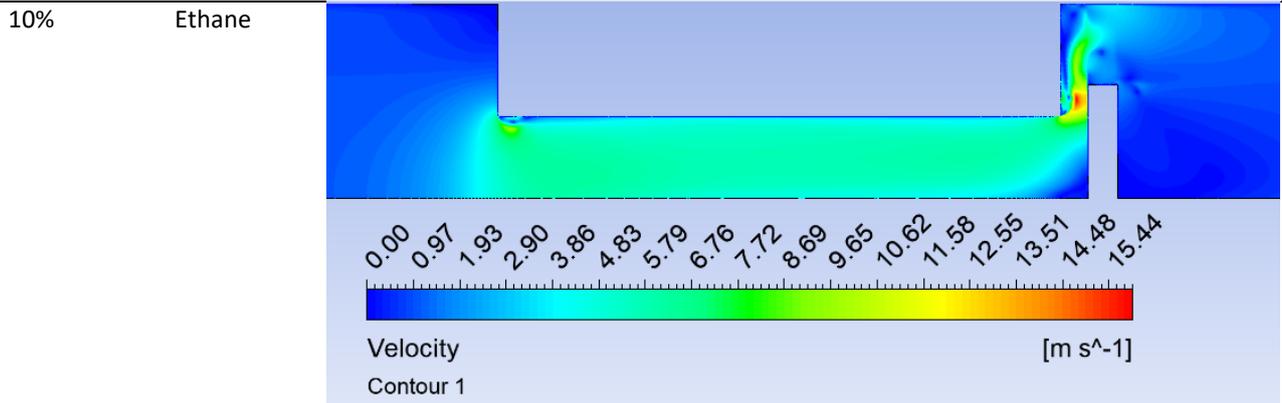
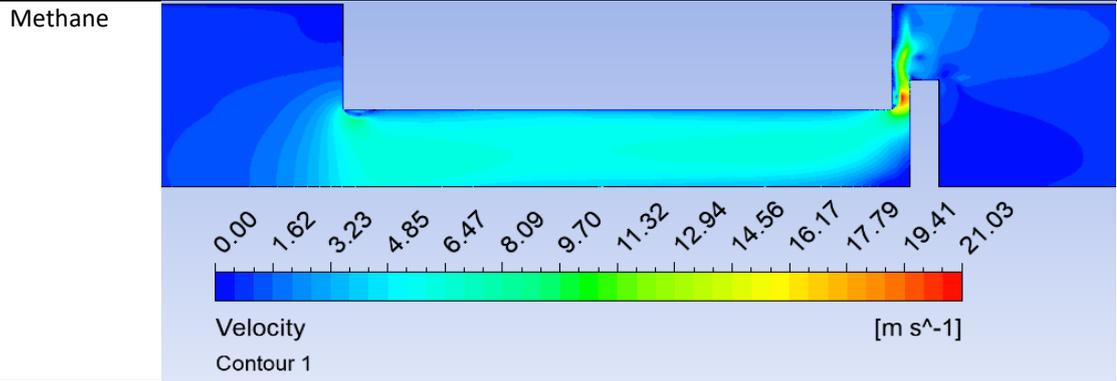
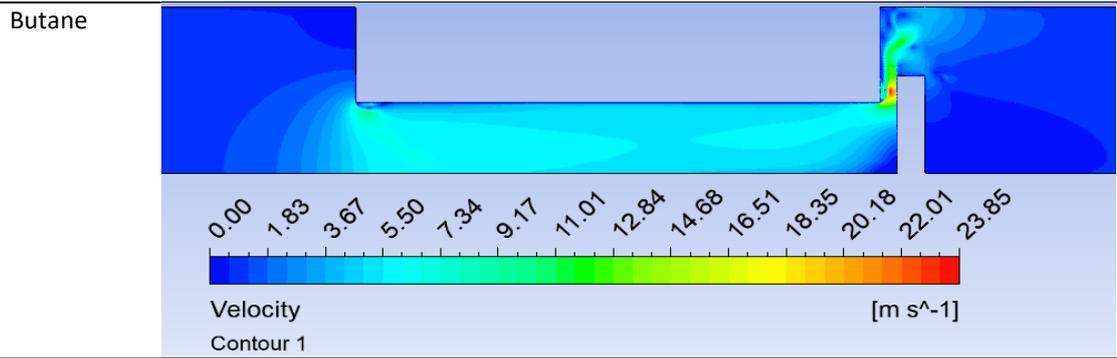
Table 4 and Table 5 illustrate the flow characteristics of the three natural gases around disk bypass PIG in terms of velocity contour and velocity streamline, respectively, for the five bypass opening percentages considered in this study. Observation on these figures indicated that the fluid velocity is higher at the horizontal bypass section than at the upstream and downstream section of the PIG. From Table 4, it can be seen that in horizontal bypass section fluid velocity reduced from 16.4 m/s to 2.71 m/s for ethane, 17.33 m/s to 2.89 m/s for butane and 15.62 m/s to 2.60 m/s for methane, respectively, at 5% bypass opening percentage. Meanwhile, at 15% bypass opening percentage the reduction in velocity was observed to be 10.16-0.63 m/s, 10.91-0.68 m/s, and 9.29-0.58 m/s for ethane, butane and methane, respectively. This shows the influence of the bypass opening percentage on reducing the fluid velocity at this section of the PIG by controlling the bypass

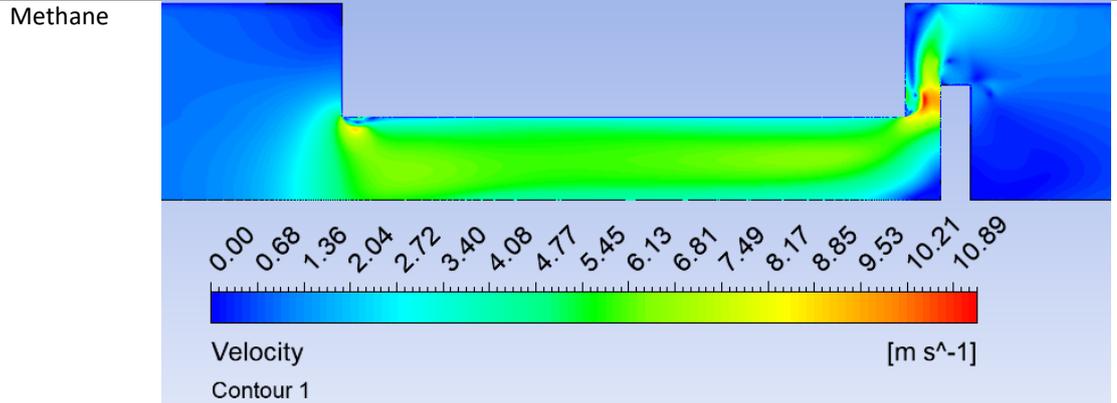
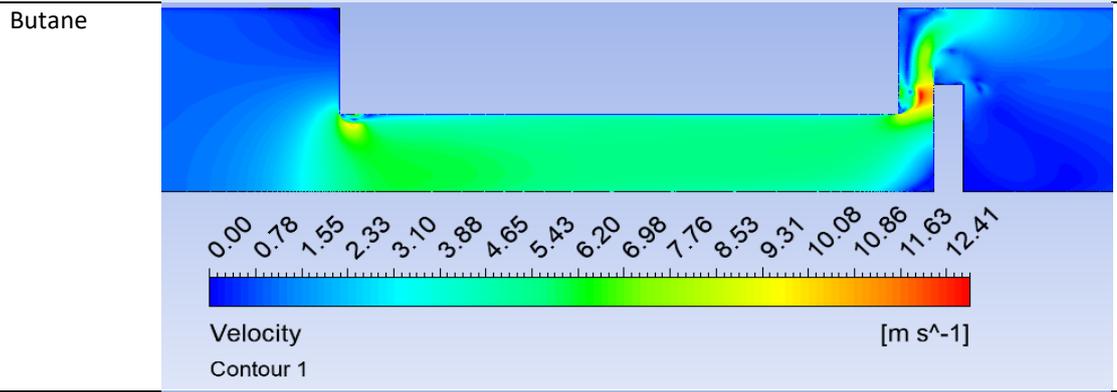
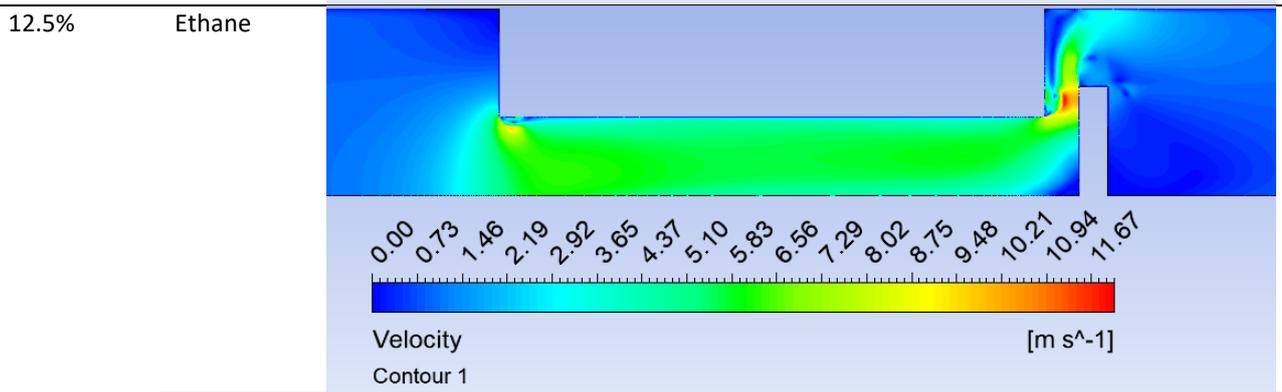
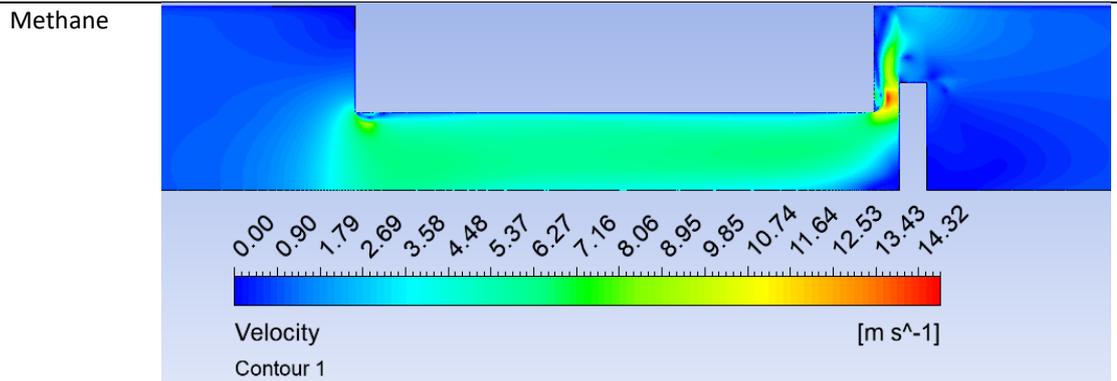
area. Additionally, these results show that among the three natural gases considered in this study, methane provided lowest ranges for velocity at horizontal bypass section compared to other natural gases.

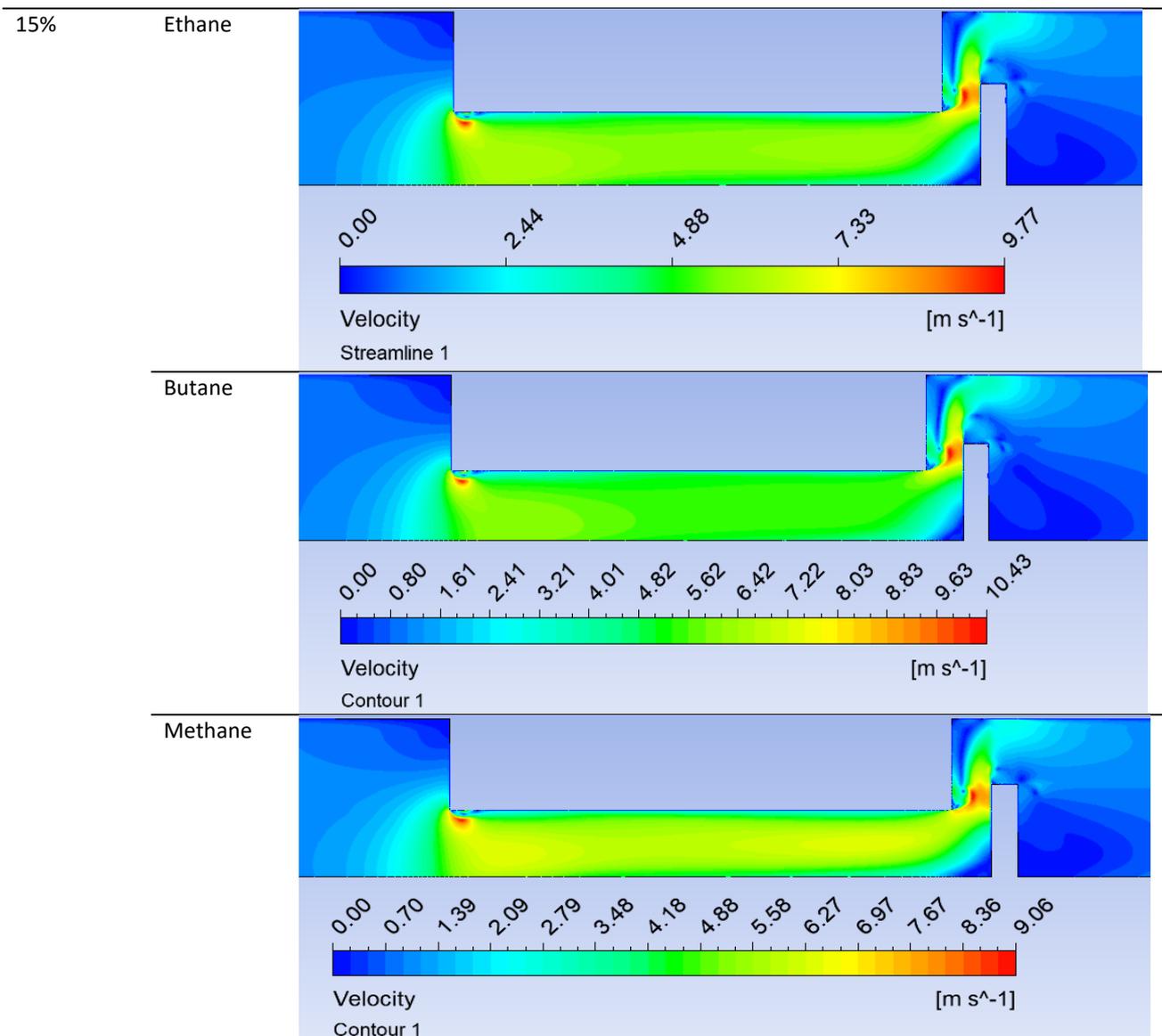
Table 4

Velocity contour of ethane, butane and methane for the five different bypass opening percentages

Bypass opening percentages	Gas	Velocity contour
5%	Ethane	 <p>Velocity Contour 1 [m s⁻¹]</p>
	Butane	 <p>Velocity Contour 1 [m s⁻¹]</p>
	Methane	 <p>Velocity Contour 1 [m s⁻¹]</p>
7.5%	Ethane	 <p>Velocity Contour 1 [m s⁻¹]</p>



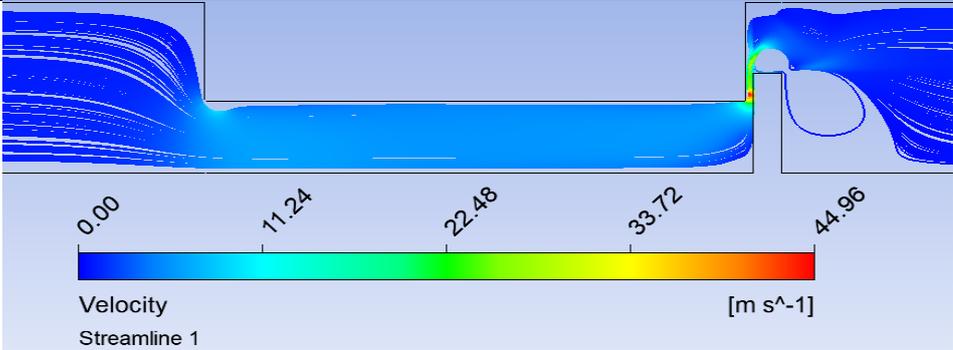
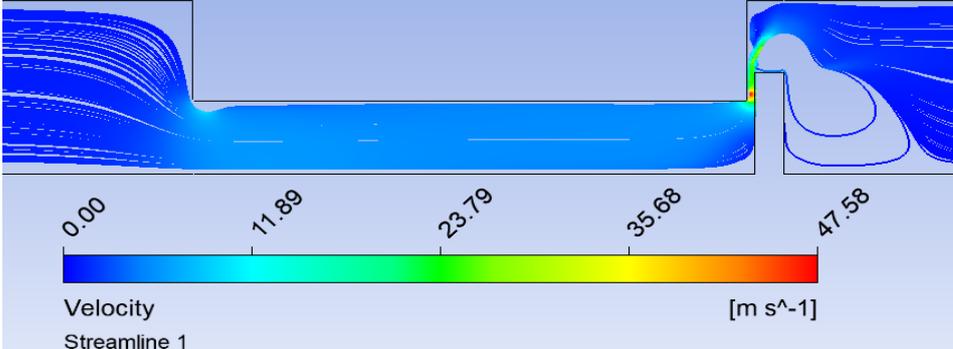
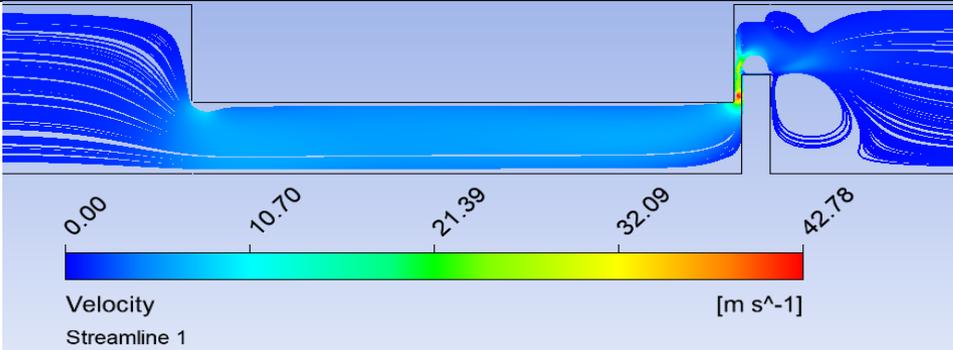
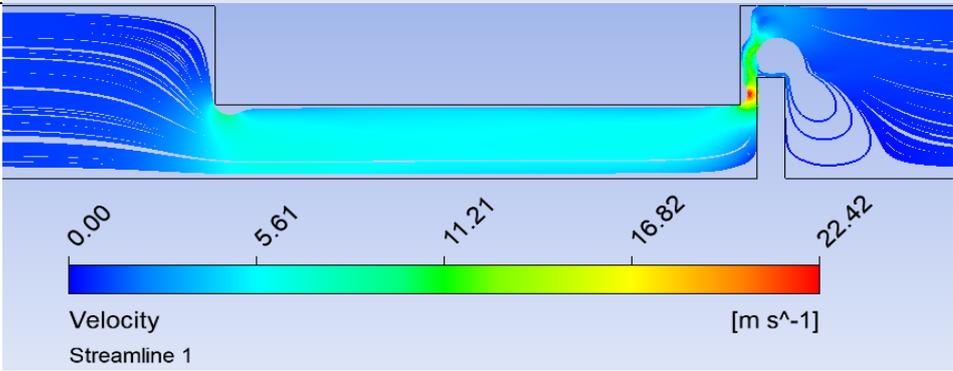


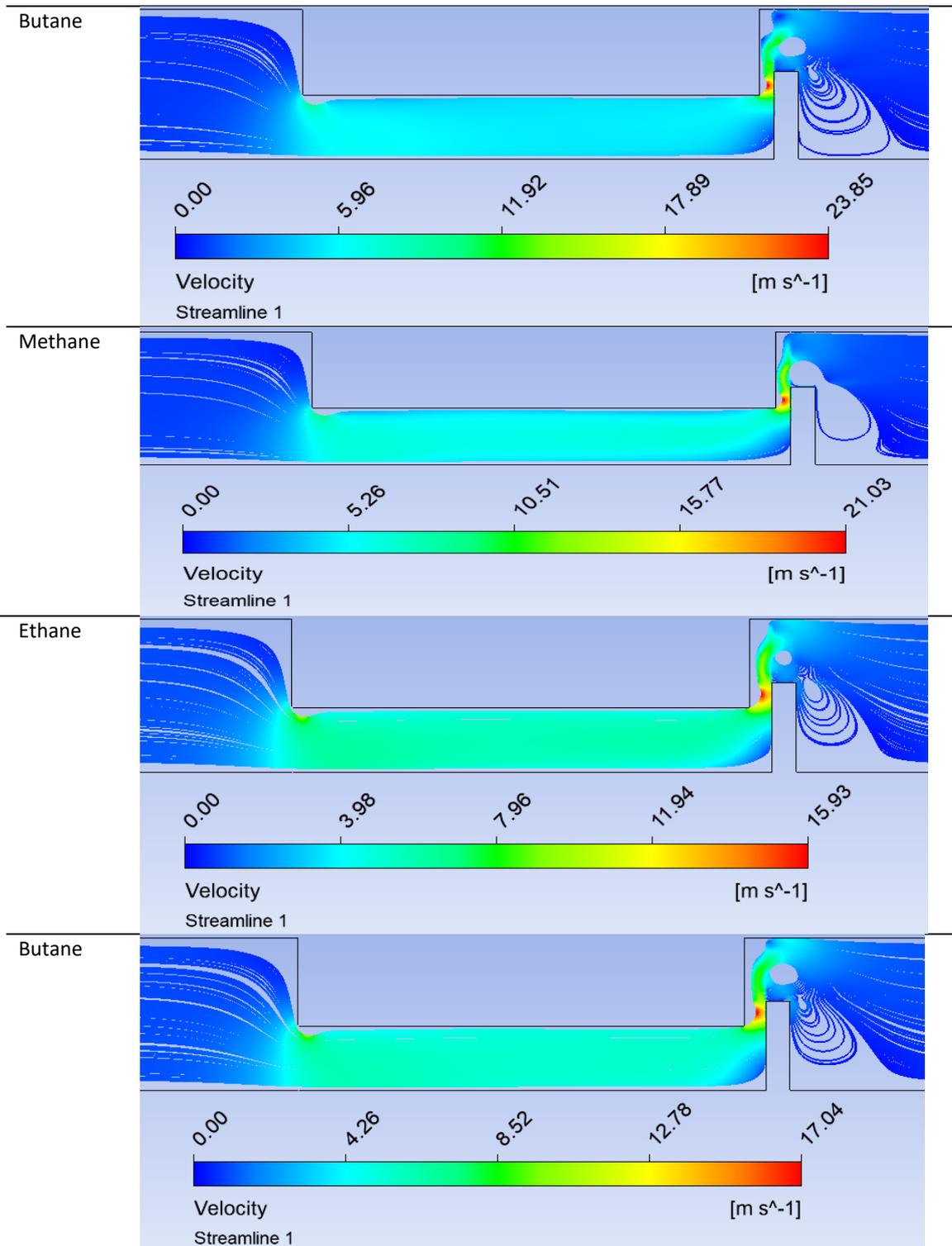


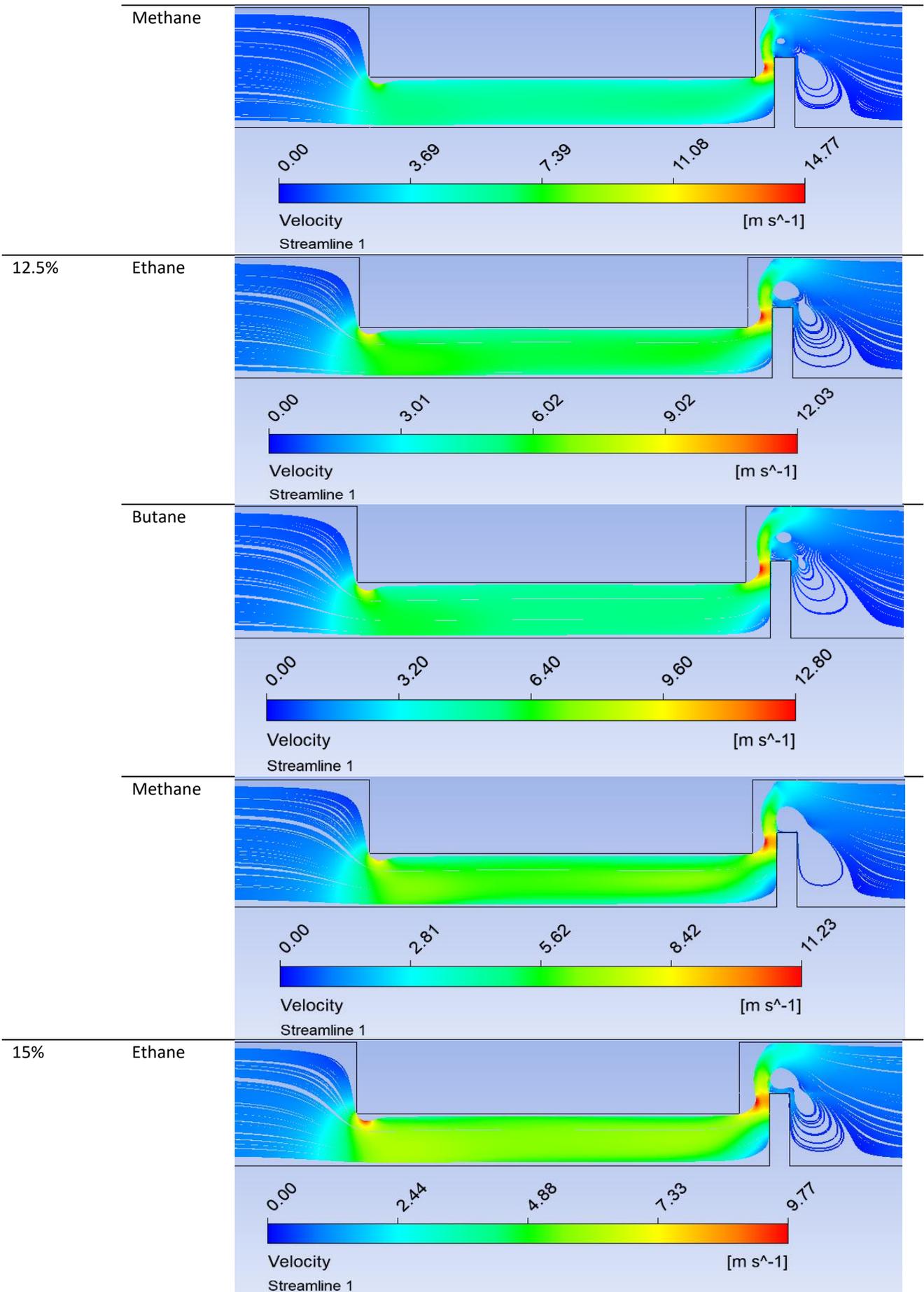
From Table 5, it was observed that at 5% bypass opening percentage, maximum fluid velocities were 44.96 m/s, 47.58 m/s and 42.78 m/s for ethane, butane and methane respectively. Meanwhile, at 15% bypass opening percentage, maximum fluid velocities were 9.97 m/s, 10.43 m/s and 9.06 m/s for these fluids, respectively. Therefore, from these results it was demonstrated that by increasing the bypass opening percentages from 5% to 15%, maximum fluid velocities reduced almost 76.6%, 76.4%, and 77.6% for these gases, respectively. Additionally, among these gases, methane provided the lowest value for maximum velocity while butane shows the highest compared to others. Table 5 also shows formation of vortices at bypass opening section. Presence of disk at bypass opening section and sudden expansion of fluid flow area created recirculation zone around disk which mainly formed vortices. Meanwhile, shear resulting from the no slip condition over boundary layers of disk, PIG and downstream wall was another key reason for the formation of these vortices. According to continuum mechanics theory, vortices have significant impact on fluid flow over a body. The streamlines in Table 5 illustrate that formation of these vorticities at the bypass opening section reduced the velocity of fluid at this section compared to bypass entry section and horizontal bypass section of the PIG.

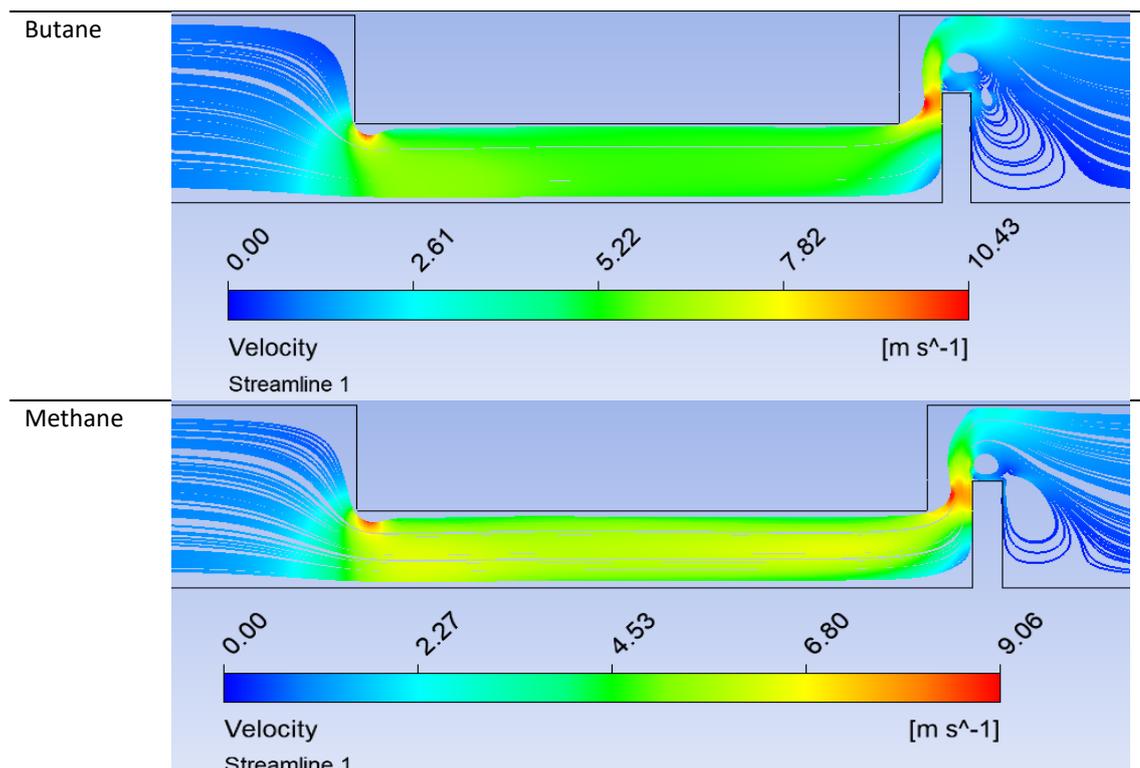
Table 5

Velocity streamline of ethane, butane and methane for the five different bypass opening percentages

Bypass opening percentages	Gas	Velocity streamline
5%	Ethane	
	Butane	
	Methane	
7.5%	Ethane	







3.2 Differential Pressure of Different Natural Gases Around Disk Bypass PIG

Figure 7 shows the differential pressure of the considered natural gases between the upstream and downstream of the PIG section as a function of the bypass opening percentage. Results demonstrated that by increasing the bypass opening percentages, differential pressure decreased for all gases. With the increase of bypass opening percentage from 5% to 15% the differential pressure has reduced 86%, 84%, and 88% for ethane, butane, and methane, respectively. At constant rate of fluid flow, smaller flow passing area results in higher fluid velocity at the inlet and outlet of the valve. This causes the fluid to generate more energy loss as it passes through the bypass valve, which in turn produces a larger pressure drop. This result is important as it indicated that the 15% bypass opening percentage performed better in terms of minimizing the differential pressure between upstream and downstream of the PIG section which is desirable for more efficient pigging operation. This finding was noted to be consistent with that for velocity reduction as discussed above. Therefore, it can be concluded that bypass opening percentage of 15% provided the best flow characteristics of the natural gases considered in this study. Additionally, methane showed a maximum 51% reduction of differential pressure compared to ethane and a 77% reduction of differential pressure compared to butane due to fluid dynamics properties of methane compared to the other gases. As seen in Table 2, methane has the lowest density and highest viscosity compared to butane and ethane, combination of which make the Reynolds number of methane being the lowest. According to fluid mechanics theory, the lower the density of the fluid, the smaller the energy loss and pressure drop. Similarly, lower Reynolds number which is a ratio of density and viscosity will also reduce the fluid velocity which causes lower energy and pressure loss in bypass opening section.

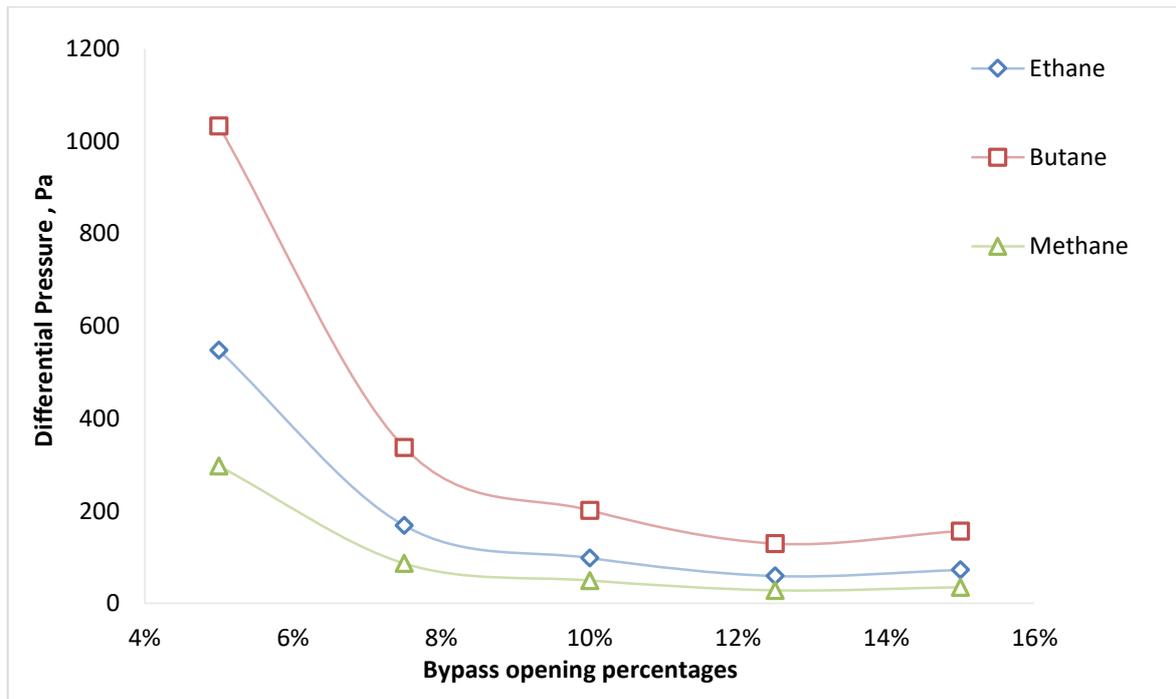


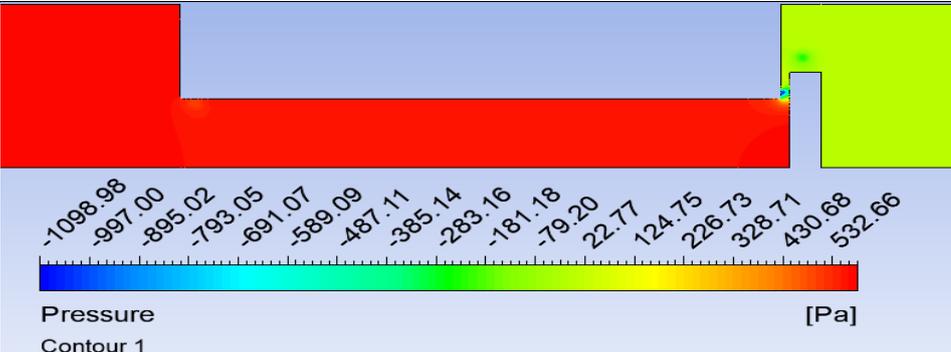
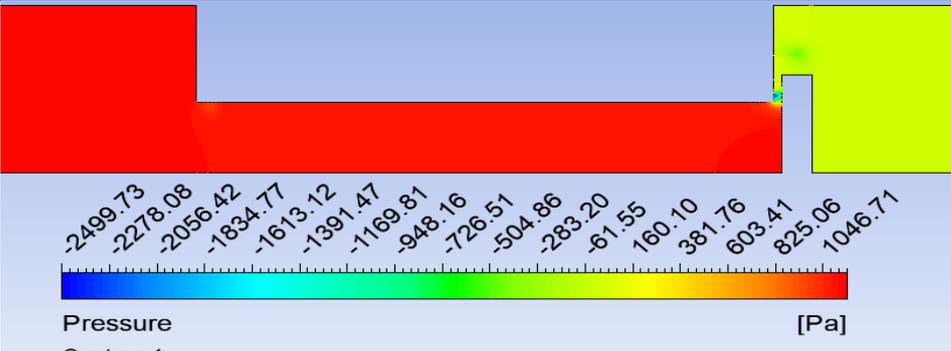
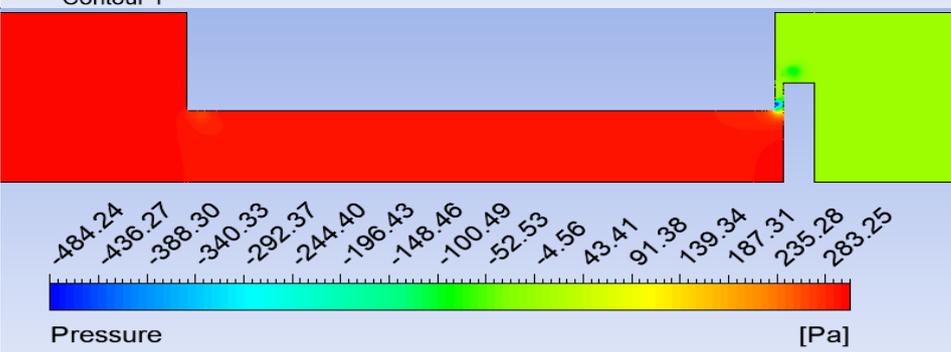
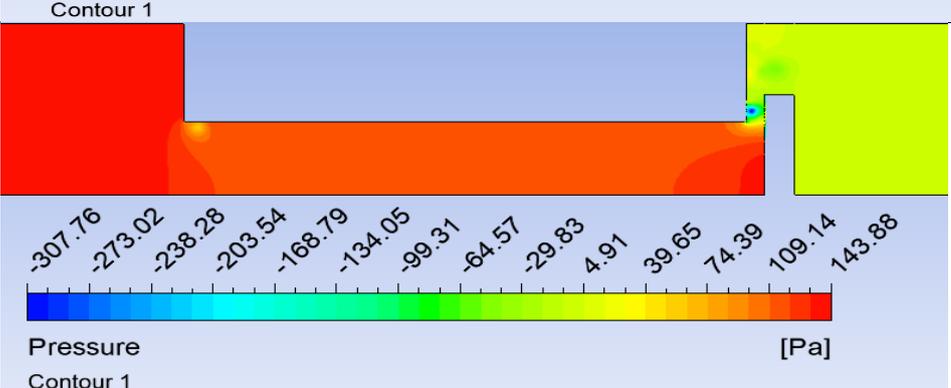
Fig. 7. Differential pressure between upstream and downstream of disk bypass PIG section as a function of bypass opening percentages for ethane, butane and methane

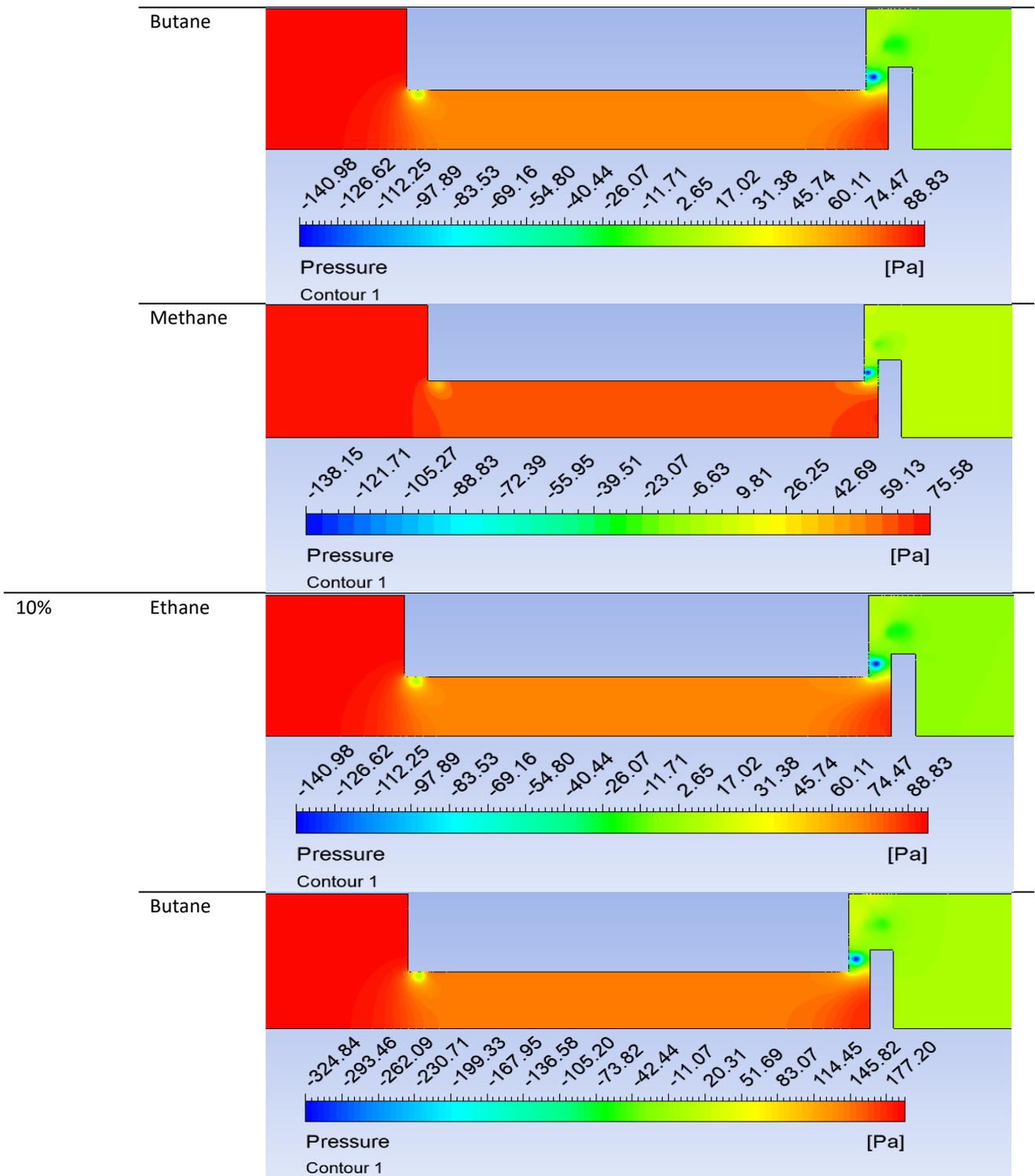
Table 6 shows the pressure contour between upstream and downstream of PIG section for the different gases at the five bypass opening percentages considered in this study. The results for all cases demonstrated the presence of high pressure at the upstream section and the horizontal bypass section. On the other hand, this high pressure was reduced at the bypass opening section and downstream section of the PIG. This reduction in pressure was due to the presence of the disk which provided obstacle to the fluid flow and therefore reduced the fluid velocity at this section. Moreover, growth of wake which mainly associated with resistance of fluid was identified at downstream. This is due to the presence of disk which created sudden contraction and expansion for the flowing fluid inside the pipe. High turbulence and density difference of the fluids are also another reason of wake. According to fluid mechanics theory, wake is important to determine drag force and other forces experienced by the body. It has significant impact on pressure loss of fluids at the bypass opening section. Growth of wake increases the pressure loss at the downstream section compared to upstream of the PIG.

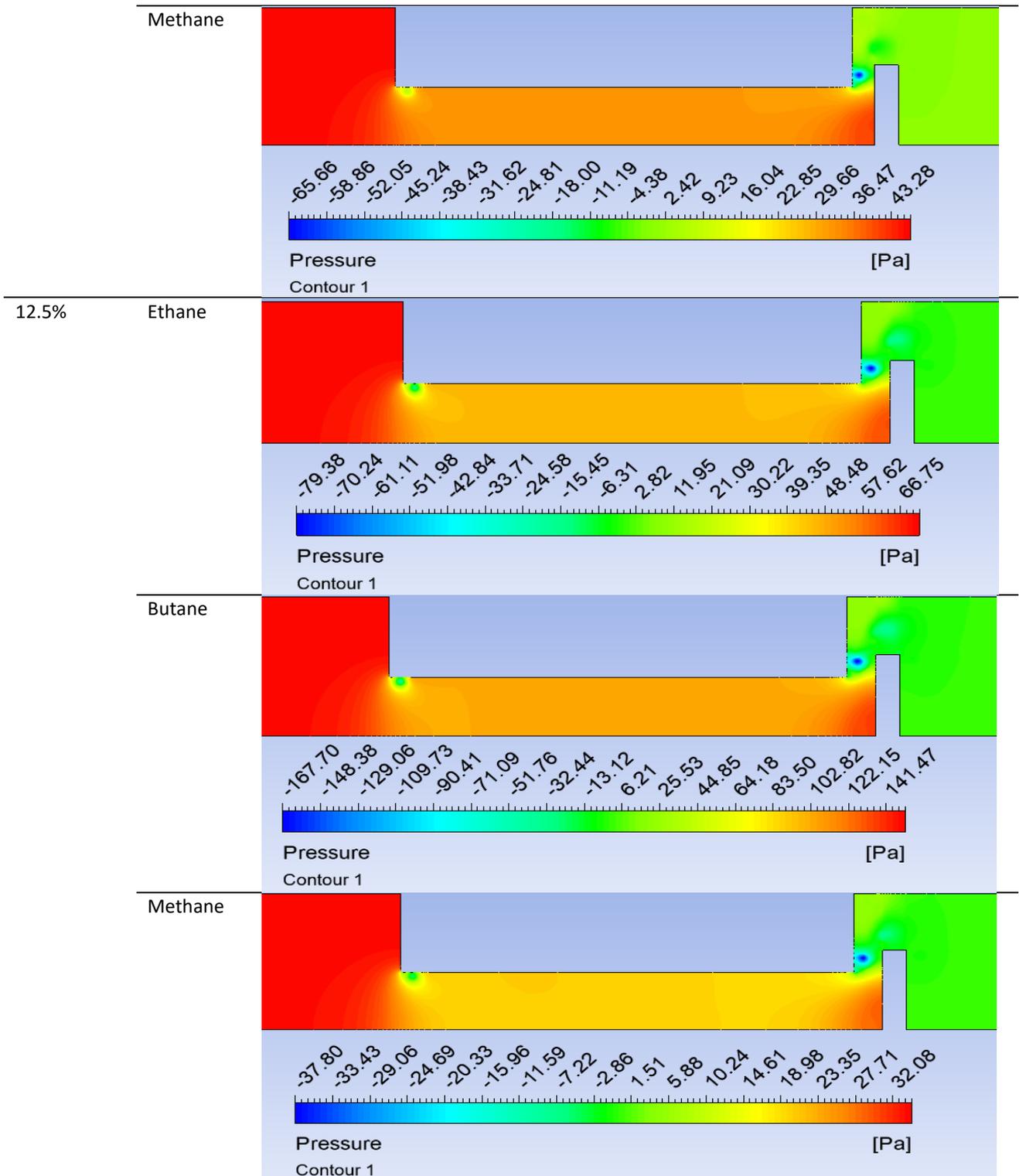
In addition, by increasing bypass opening percentages from 5% to 15% maximum pressure has reduced almost 88%, 86%, and 89% for ethane, butane, and methane, respectively. Additionally, methane provided the lowest pressure value in the pressure contour due to the fluid dynamics properties of methane compared to the other gases.

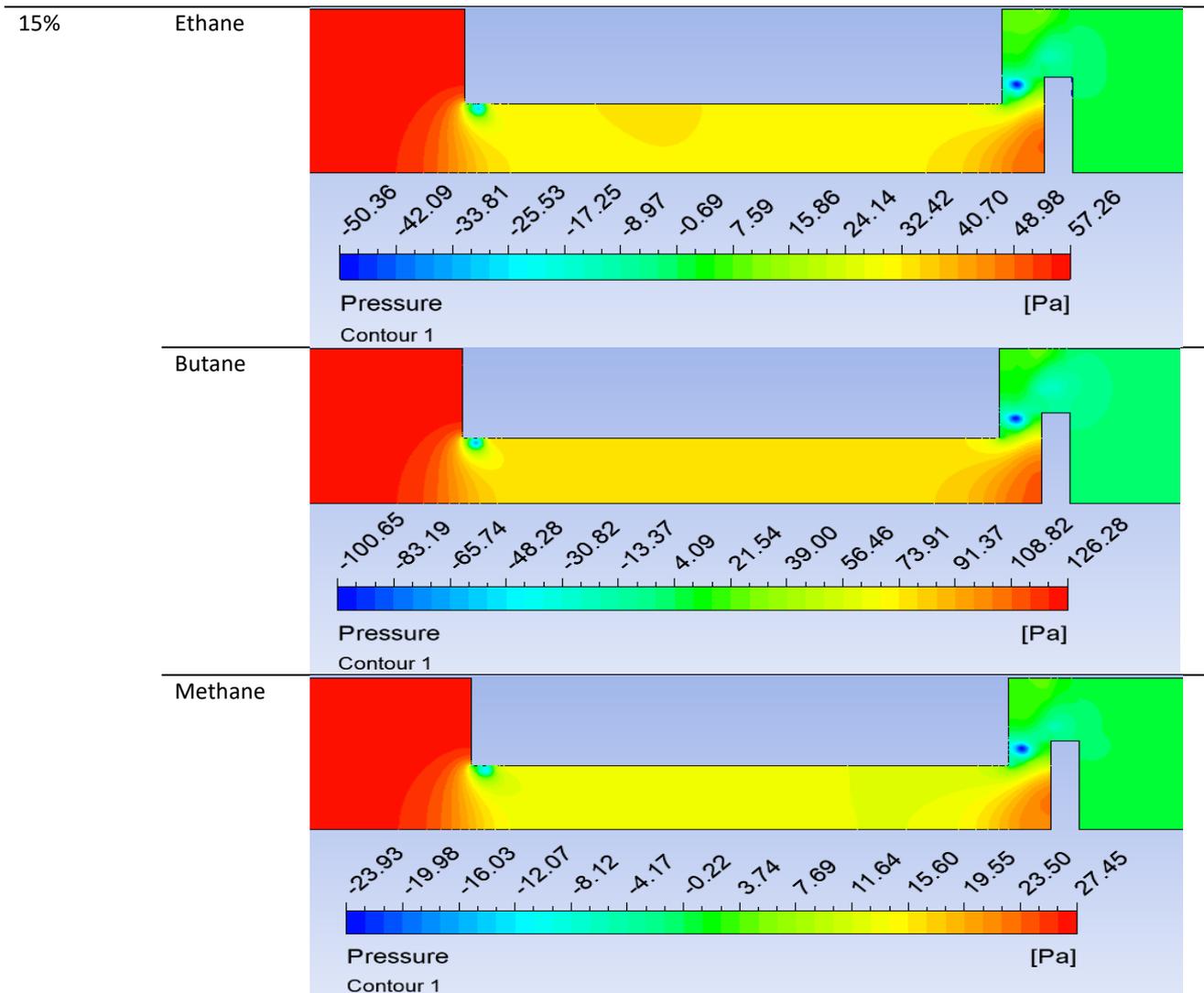
Table 6

Pressure contour of ethane, butane and methane for the five different bypass opening percentages

Bypass opening percentages	Gas	Pressure contour
5%	Ethane	 <p>Pressure Contour 1 [Pa]</p>
	Butane	 <p>Pressure Contour 1 [Pa]</p>
	Methane	 <p>Pressure Contour 1 [Pa]</p>
7.5%	Ethane	 <p>Pressure Contour 1 [Pa]</p>







The summaries of the main findings from this study in terms of the velocities and differential pressure of the natural gases around the disk bypass PIG are presented in Table 7 and Table 8. Table 7 represents the comparison of reduction percentage for maximum fluid velocity at horizontal bypass section (v_2) and at bypass opening section (v_3) as well as the differential pressure over the PIG section among ethane, methane, and butane for increasing bypass opening percentages from 5% to 15%. The reduction percentages were calculated by applying the following equation:

$$\text{Reduction percentages (\%)} = \frac{\text{value at 5\%} - \text{value at 15\%}}{\text{value at 5\%}} \times 100\% \quad (11)$$

The results demonstrated that as the bypass opening percentage increased from 5% to 15%, the velocities of all gases at horizontal bypass section and bypass opening section reduced. This result indicated that 15% bypass opening percentage provided lowest velocities at these sections and therefore is more desirable as compared to other bypass opening percentage values considered in this study. Likewise, for differential pressure, the results shown in Table 7 demonstrates that the differential pressure reduced significantly with 15% bypass opening percentage compared to the others. Therefore, it can be concluded that flow characteristics in terms of velocities and differential pressure for all gases were the best at 15% bypass opening percentage.

Table 7

Reduction percentage (%) for ethane, methane and butane by increasing bypass opening percentages from 5% to 15%

Parameters	Ethane	Butane	Methane
Fluid velocity at horizontal bypass section, v_2	2.1	1.3	2.3
Fluid velocity at the bypass opening section, v_3	28.28	40.43	21.21
Differential pressure	88	86	89

Meanwhile, Table 8 shows the results comparison among ethane, methane, and butane for the best opening percentage considered in this study which was found to be 15%. From this table, methane resulted in the lowest fluid velocity of v_2 and v_3 compared to ethane and butane. Additionally, differential pressure of methane was also found to be the lowest at this percentage compared to other gases. On the other hand, butane shows the highest values of these results. Therefore, it can be predicted that during pigging operation, the PIG would perform with the lowest speed and result in lowest differential pressure inside methane flowing pipelines compared to ethane and butane.

Based on these key findings, it can be concluded that flow characteristics in terms of velocities and differential pressure were the best at 15% bypass opening percentage with methane as the fluid compared to other cases.

Table 8

Flow characteristics of ethane, methane and butane at 15% bypass opening percentages

Variables	Ethane (15%)	Butane (15%)	Methane (15%)
Reynolds Number	58786	151958	26569
Fluid velocity at horizontal bypass section, v_2 (m/s)	5.08	5.27	4.80
Fluid velocity at the bypass opening section, v_3 (m/s)	0.79	0.85	0.76
Differential pressure (Pa)	72.65	156.65	34.95

3.3 Correlation of Differential Pressure

In order to predict differential pressure between upstream and downstream section of the PIG which essentially drives the PIG forward, a correlation was developed by using curve fitting of data in this study that enables quick prediction of this important flow characteristics in future use. The developed correlation is a function of various parameters of the PIG geometry including the bypass opening percentage as well as gas density and inlet velocity, which is given by

$$\Delta P = \left(\frac{L_{PIG}}{D} \rho \frac{v_{in}^2}{2} \right) \left(\frac{H}{d} \right)^a h \quad (12)$$

where D is pipe diameter; d is horizontal bypass PIG diameter; h is bypass opening percentages; H is disk diameter; L_{PIG} is horizontal bypass length of PIG; ρ is the gas density; and v_{in} is the inlet velocity of the gas.

Meanwhile, a in Eq. (12) is a correlation factor and the values are given in Table 9 for different h values.

Table 9
 Values of correlation factor (a) for different h conditions

h (%)	a
5	29.5
7.5	24.6
10	22
12.5	20.5
15	19.4

Figure 8 demonstrates comparison between results from the developed correlation and simulations for ethane, butane and methane. It can be seen from this figure that the results from developed correlation provided similar trend with the simulation results. The percentage of maximum deviation was 3.8% for ethane, 7.7% for butane, and 6.6% for methane, respectively. Moreover, the root mean square error (RMSE) between the correlation and simulation results was obtained to be 0.44 for ethane, 0.52 for butane and 0.49 for methane, respectively. The observed maximum deviation and RMSE values indicated good agreement between correlation and simulation results. Therefore, it can be concluded that the developed correlation in this study can be used to predict the differential pressure of gases around disk bypass PIG under the conditions considered in this study.

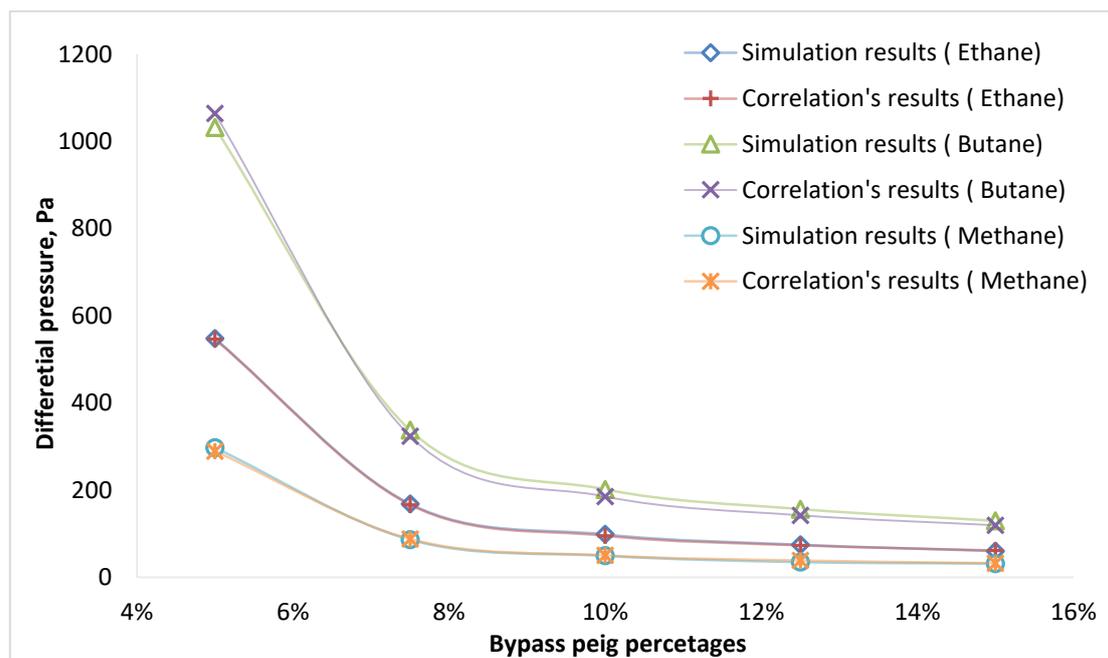


Fig. 8. Comparison of correlation and simulation results for differential pressure as a function of bypass opening percentages for ethane, butane and methane

4. Conclusions

Flow characteristics of methane, ethane and butane around disk bypass PIG were analysed in this study using computational fluid dynamics approach. The key findings from this study are the following.

- a) With the increase of bypass opening percentages 5% to 15%, fluid velocity at bypass opening section has reduced 28.28%, 40.43%, and 21.21% for ethane, butane, and methane, respectively, while the differential pressure has reduced 88%, 86%, and 89% for these natural

gases, respectively. This key finding indicated that bypass opening percentage of 15% provided the best flow characteristics in terms of both velocity and differential pressure in comparison to other percentages considered in this study.

- b) At 15% bypass opening percentage, methane resulted in the lowest fluid velocity at bypass opening section compared to ethane and butane. Additionally, methane also resulted in lowest differential pressure at this percentage compared to other gases. Therefore, it can be concluded that flow characteristics in terms of velocities and differential pressure were the best at 15% bypass opening percentage with methane as the fluid compared to other cases.
- c) A correlation of differential pressure was also developed for first time in this study that can be used to predict differential pressure of natural gases around disk bypass PIG under the conditions considered in this study. The developed correlation agreed well with simulation results with maximum deviation of 3.8% for ethane, 7.7% for butane, and 6.6% for methane.

Acknowledgement

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